

# Boom clay drying behavior: experimental and numerical study

J. Hubert <sup>1</sup> – N. Prime <sup>3</sup> – E. Plougonven <sup>2</sup> – A. Leonard <sup>2</sup> – F. Collin <sup>1</sup>

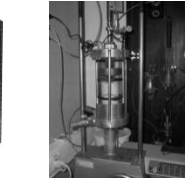
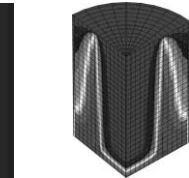
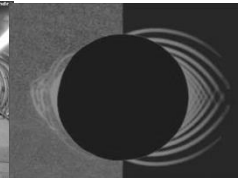
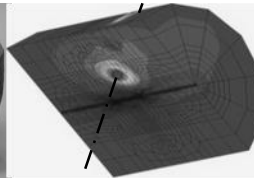
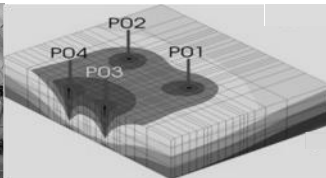
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<sup>2</sup> Université de Liège – Dept. Chimie appliquée

<sup>3</sup> Université Savoie Mont-Blanc LOCIE

Thesis director : Frédéric Collin

*Wednesday 25<sup>th</sup> of May*

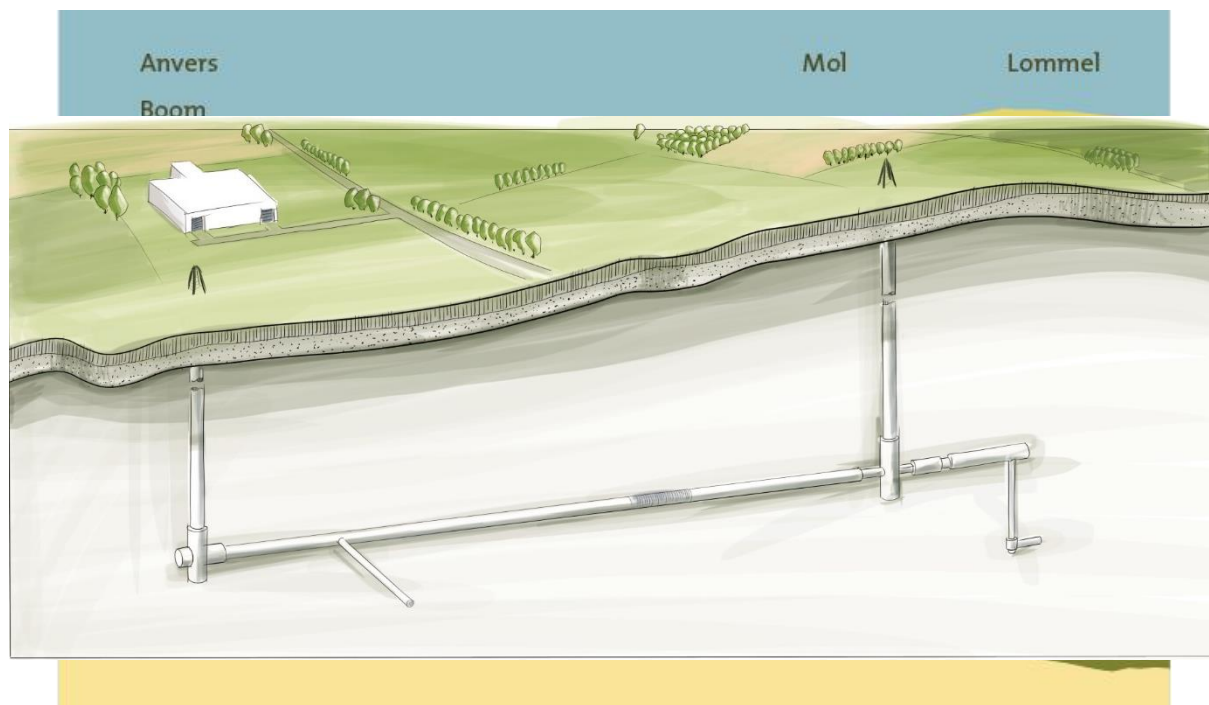


# SUMMARY OF THE PRESENTATION

- Nuclear waste disposal
- Material and method
- Drying kinetics
- Shrinkage
- Conclusions

# NUCLEAR WASTE DISPOSAL

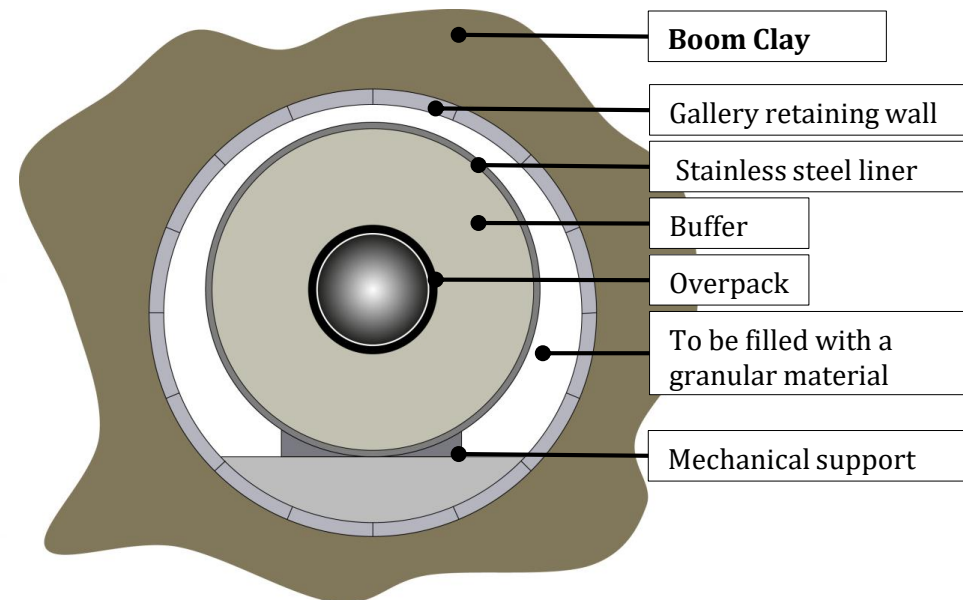
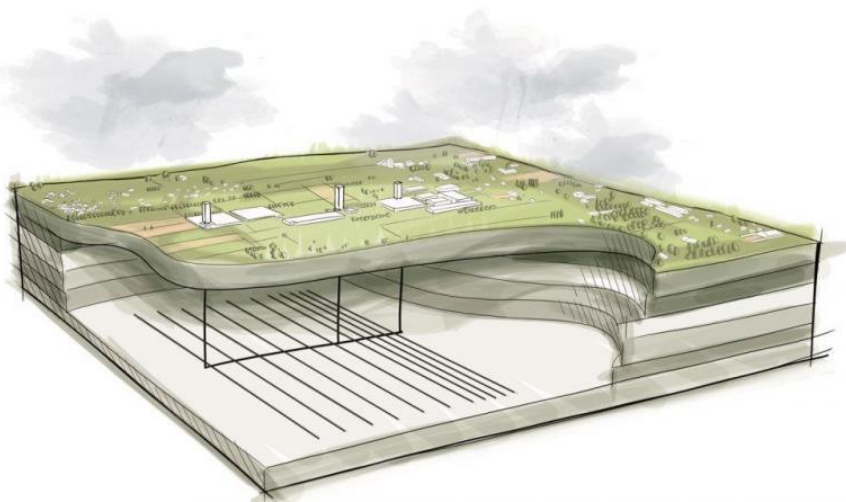
- High activity long life **radioactive wastes** need to be **isolated** for a **long period of time** ⇒ **Deep geological disposal**
  - Stable and low permeability rock formation required  
⇒ in **Belgium** the studied formation is **Boom Clay**



ONDRAF

# NUCLEAR WASTE DISPOSAL

- Deep geological storage
  - Burial shaft and multi barrier principle:



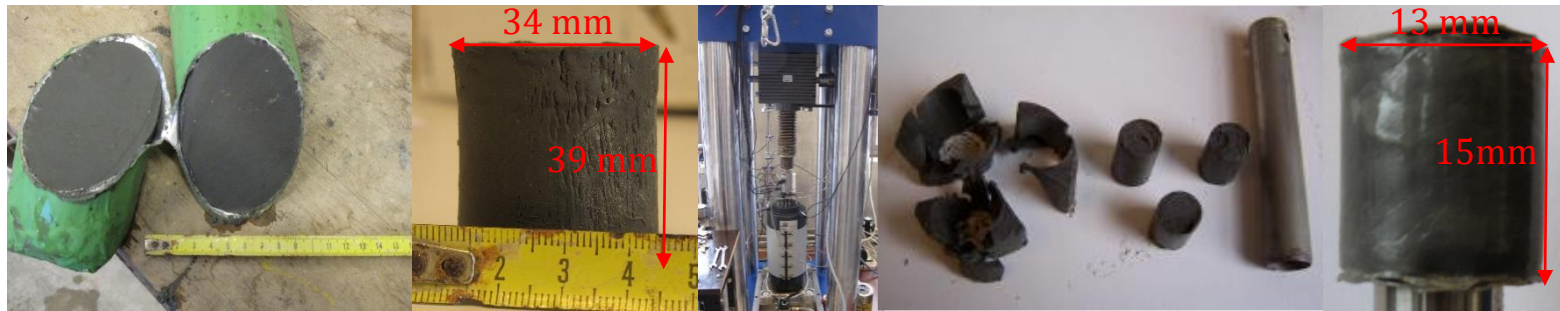
*Craye et al., 2009*

# SUMMARY OF THE PRESENTATION

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# MATERIAL AND METHOD

- Samples preparation



Initial core

Extracted  
samples

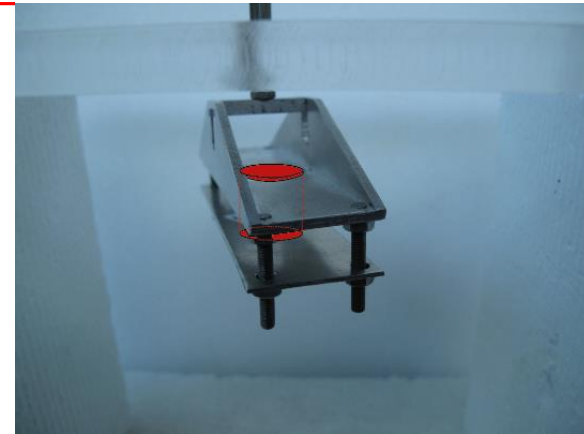
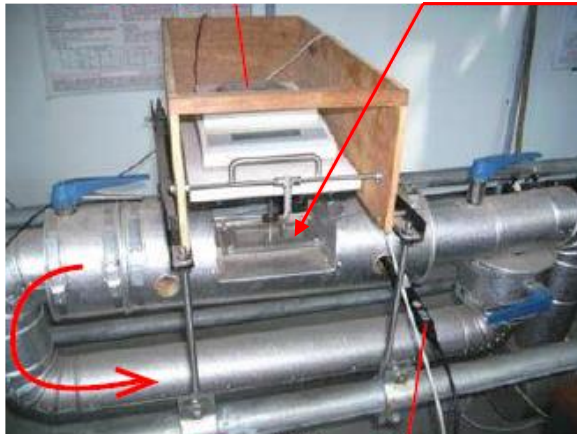
Saturation

Optimization

Finished samples

# MATERIAL AND METHOD

- Convective drying test
  - Sample weighed every 30 seconds in the convective dryer



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## Drying conditions

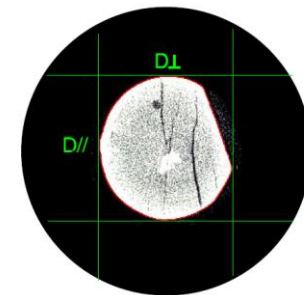
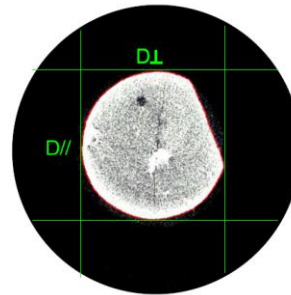
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Temperature	25°C
Humidity	3,5 %
Air flow	0,8 m/s

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# MATERIAL AND METHOD

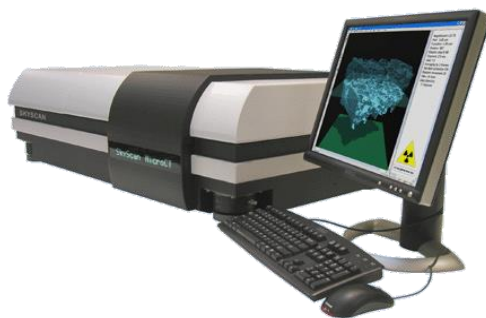
- Data acquisition and image processing
  - Shrinkage and cracking measurement



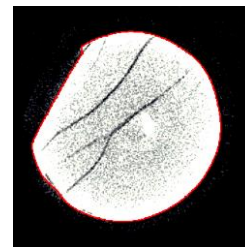
Identification of the bedding direction

Dimensions at saturated state

Dimensions until dry state



*Skyscan 1172*



Hole filling and binarization



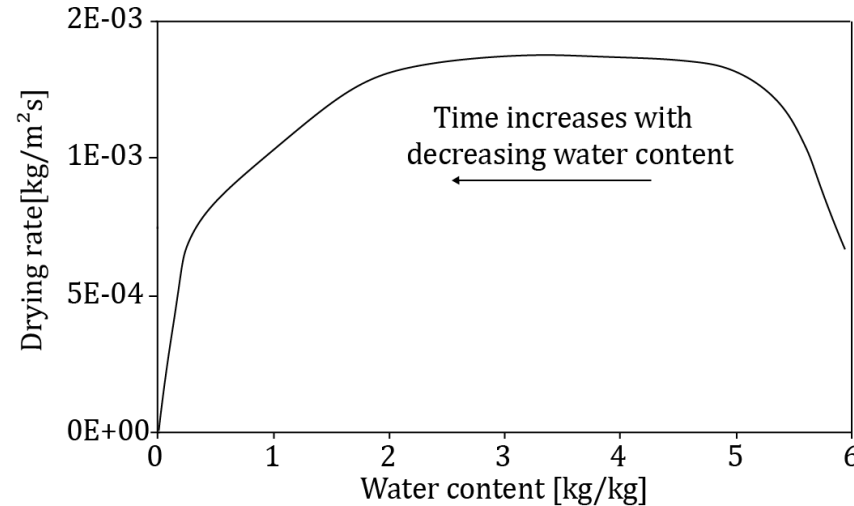
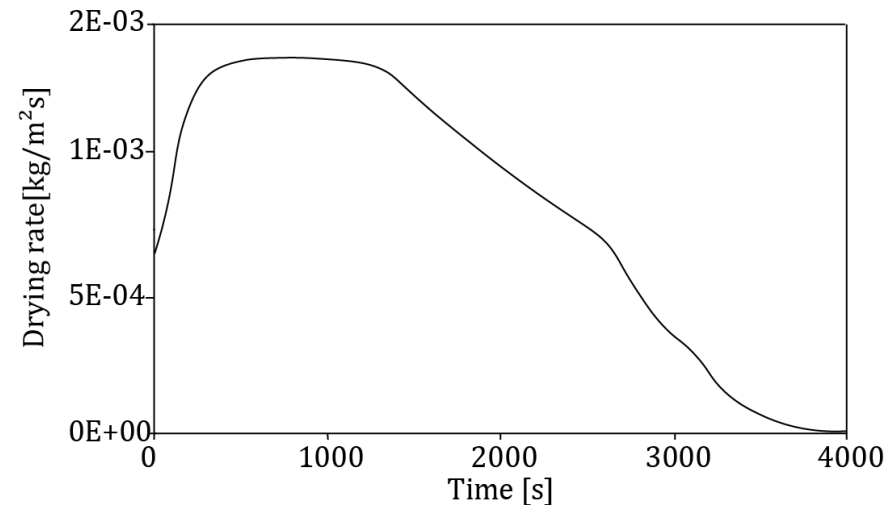
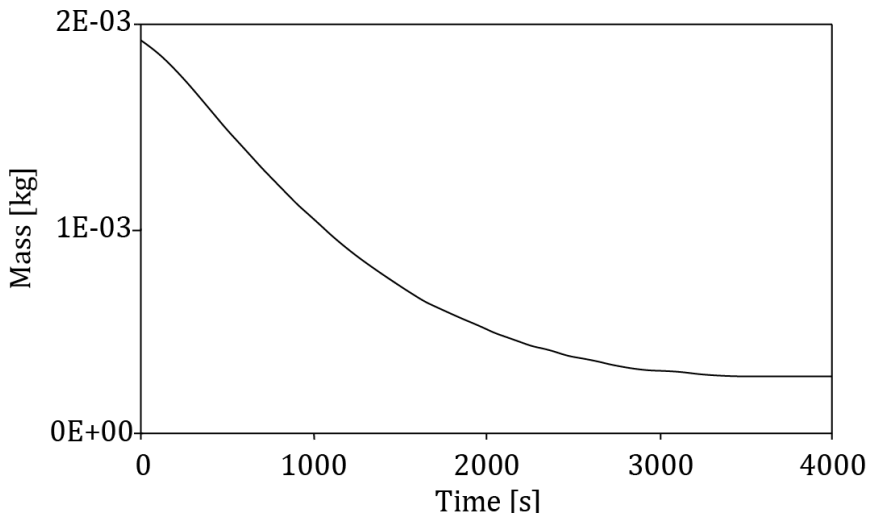


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# DRYING KINETICS

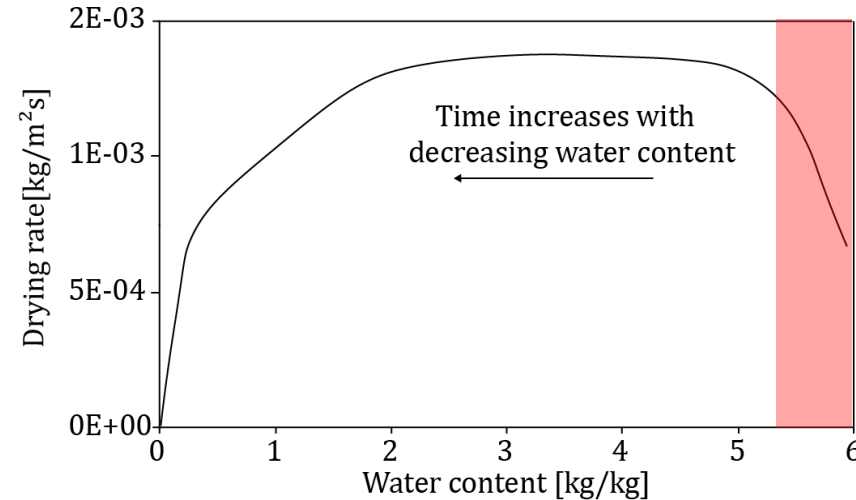
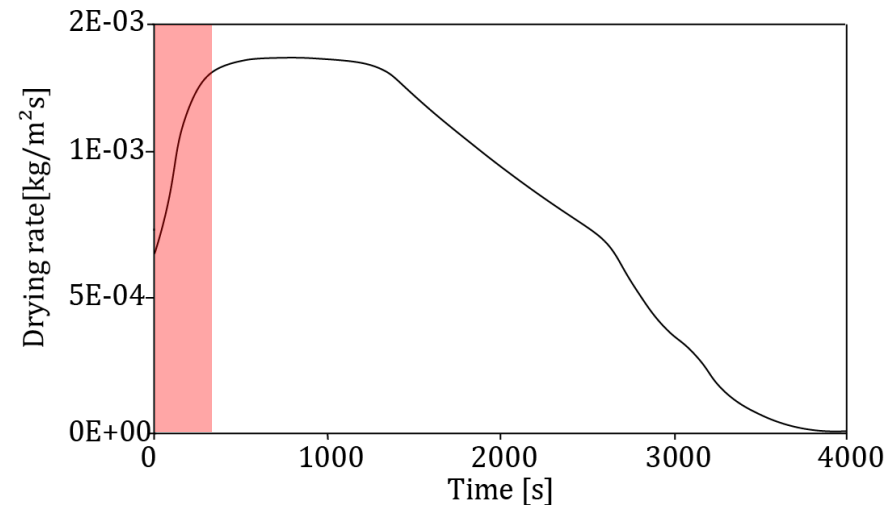
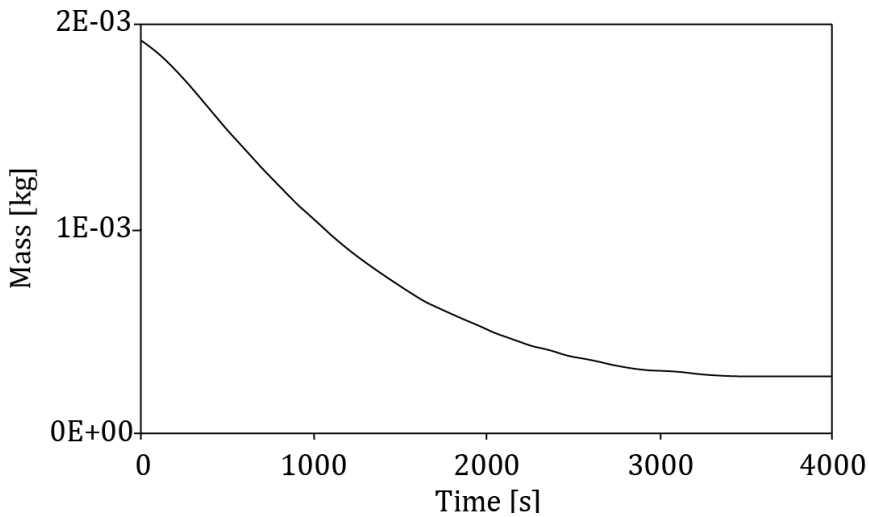
- Theory of porous media drying kinetics



Léonard, 2002

# DRYING KINETICS

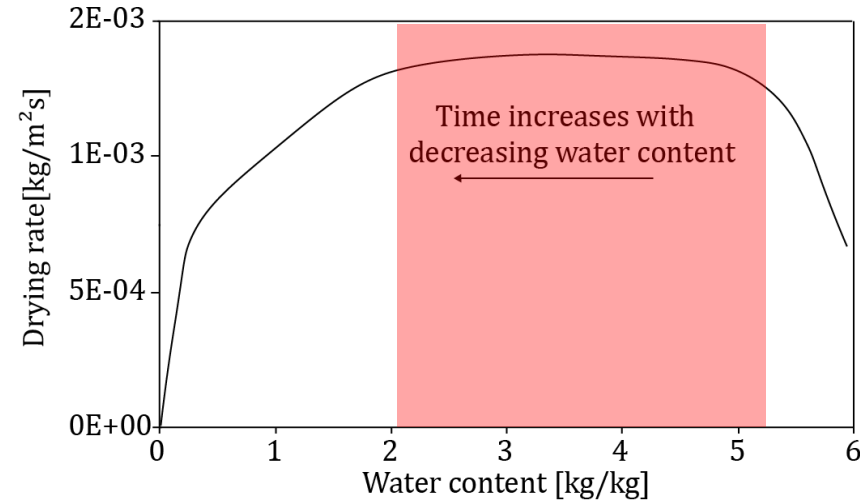
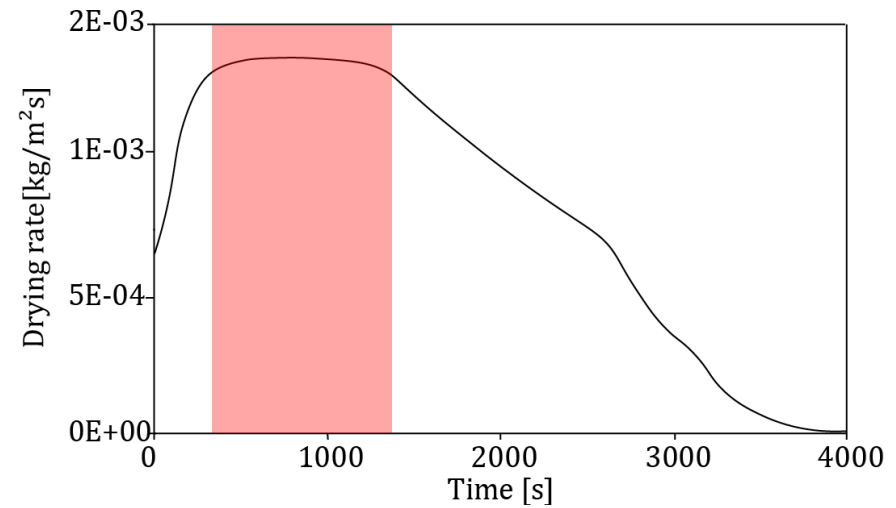
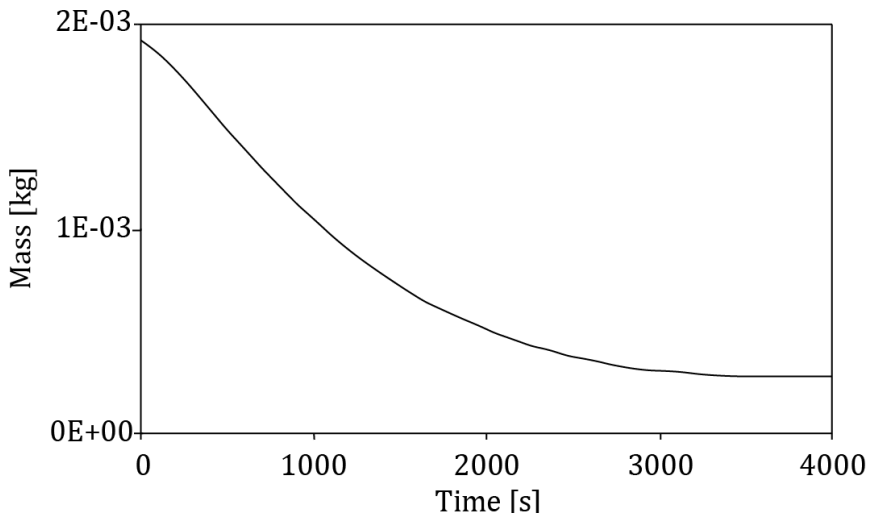
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Léonard, 2002

# DRYING KINETICS

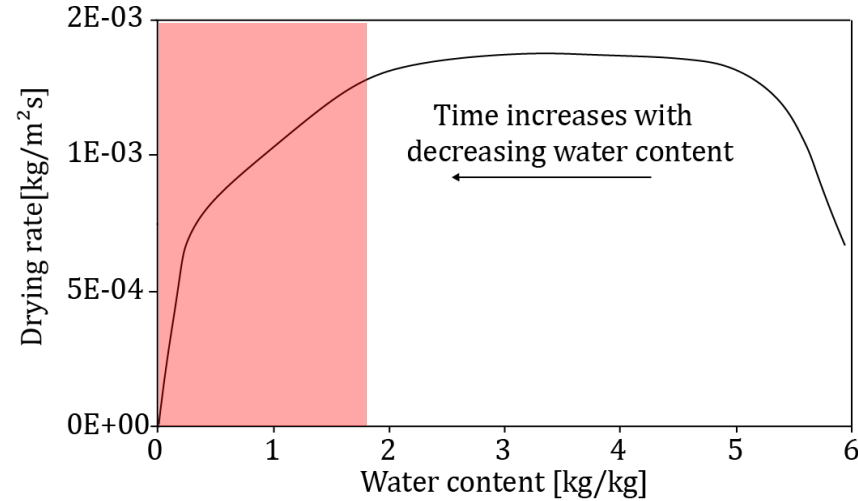
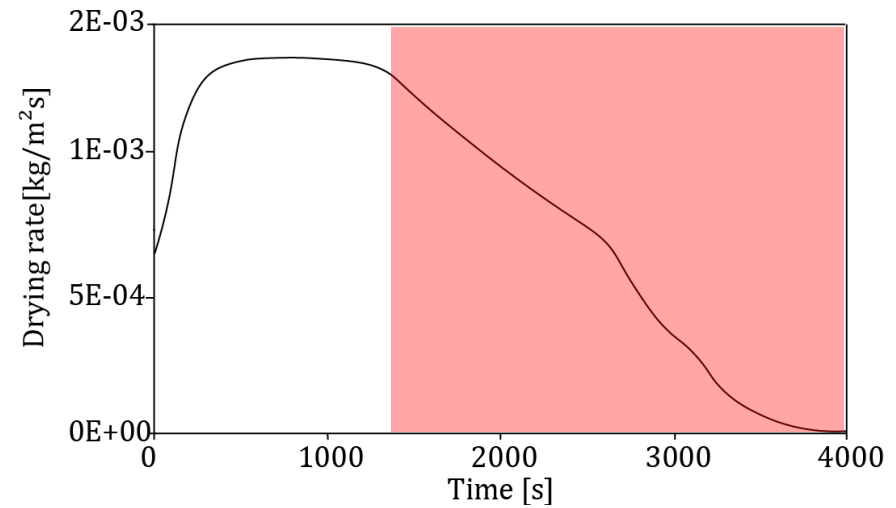
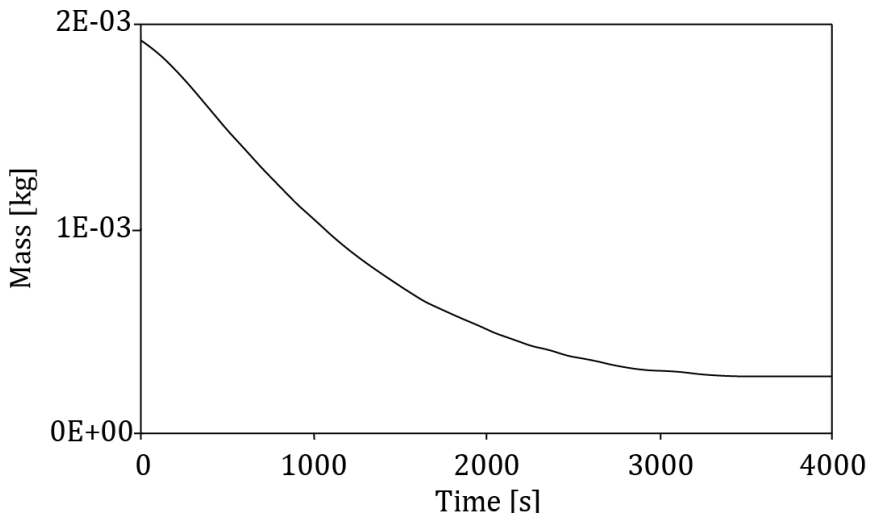
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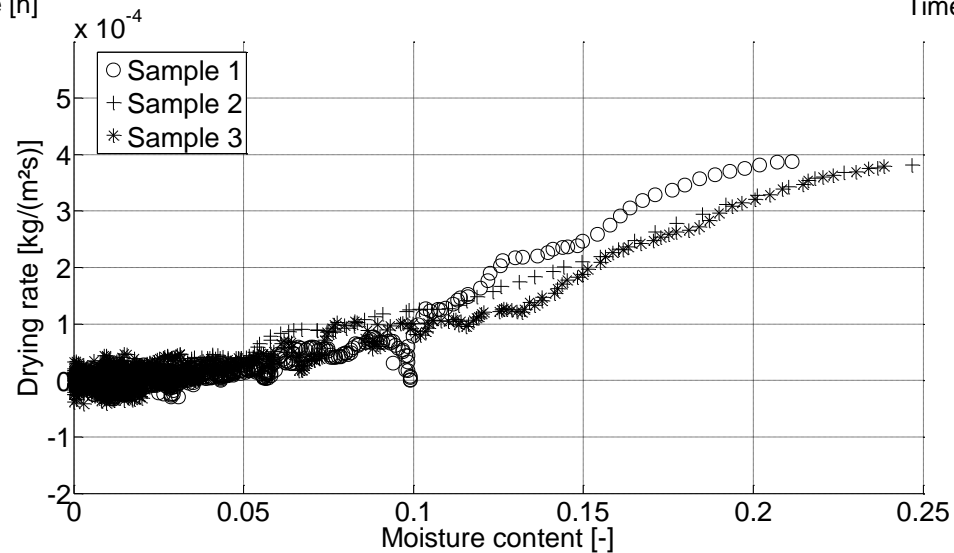
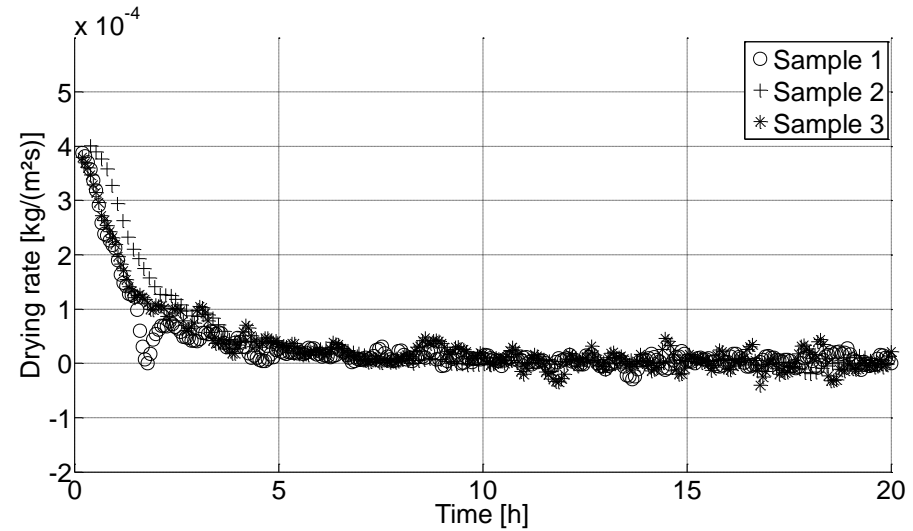
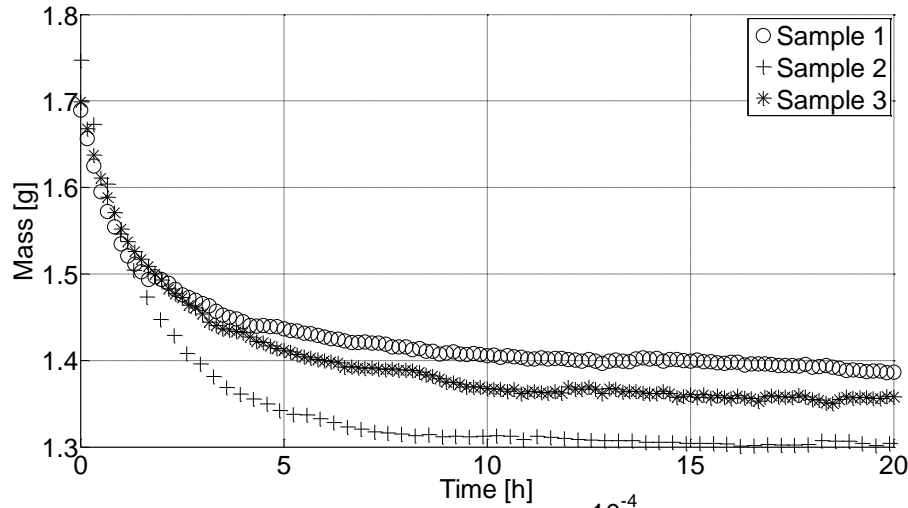
- Theory of porous media drying kinetics



Léonard, 2002

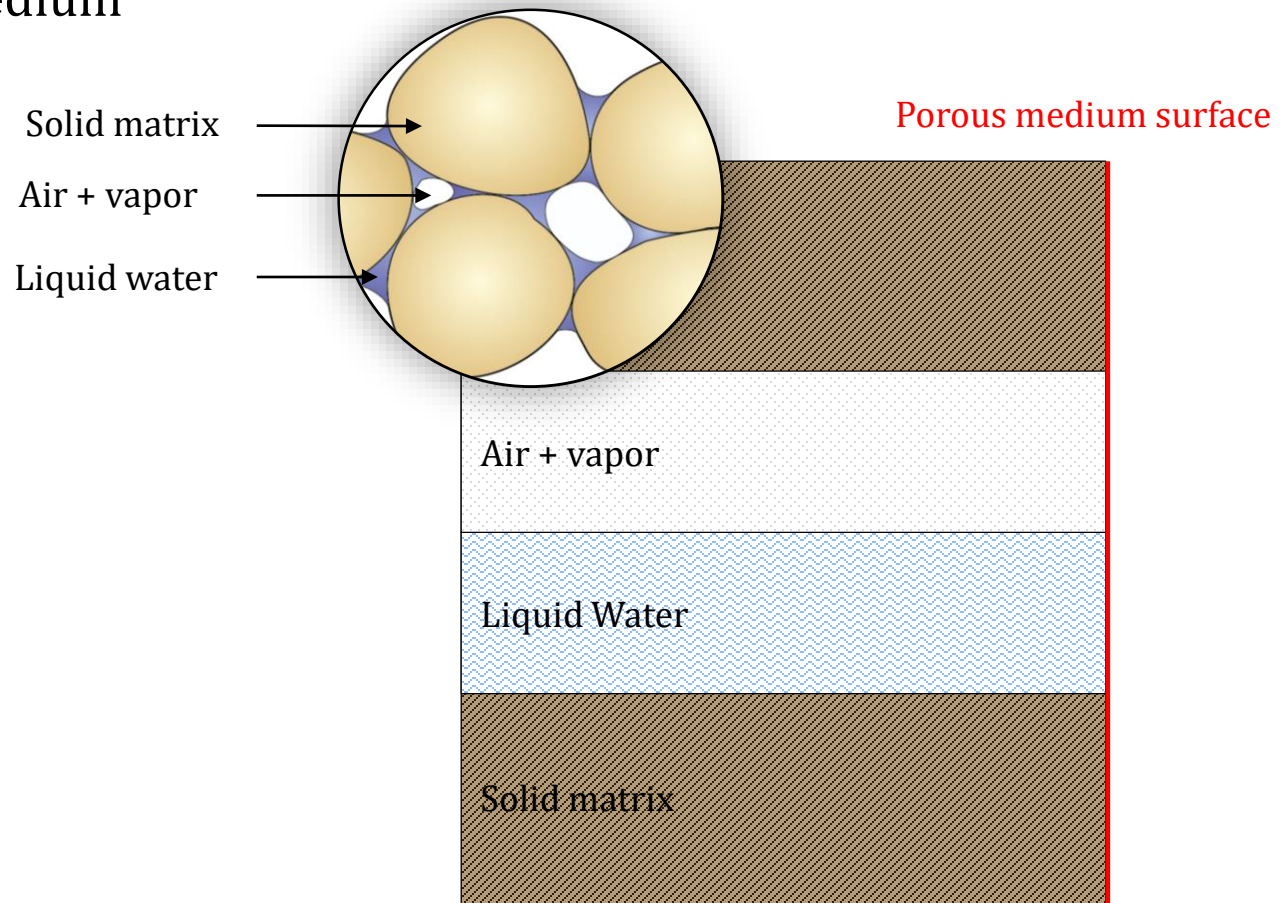
# DRYING KINETICS

## ■ Experimental results



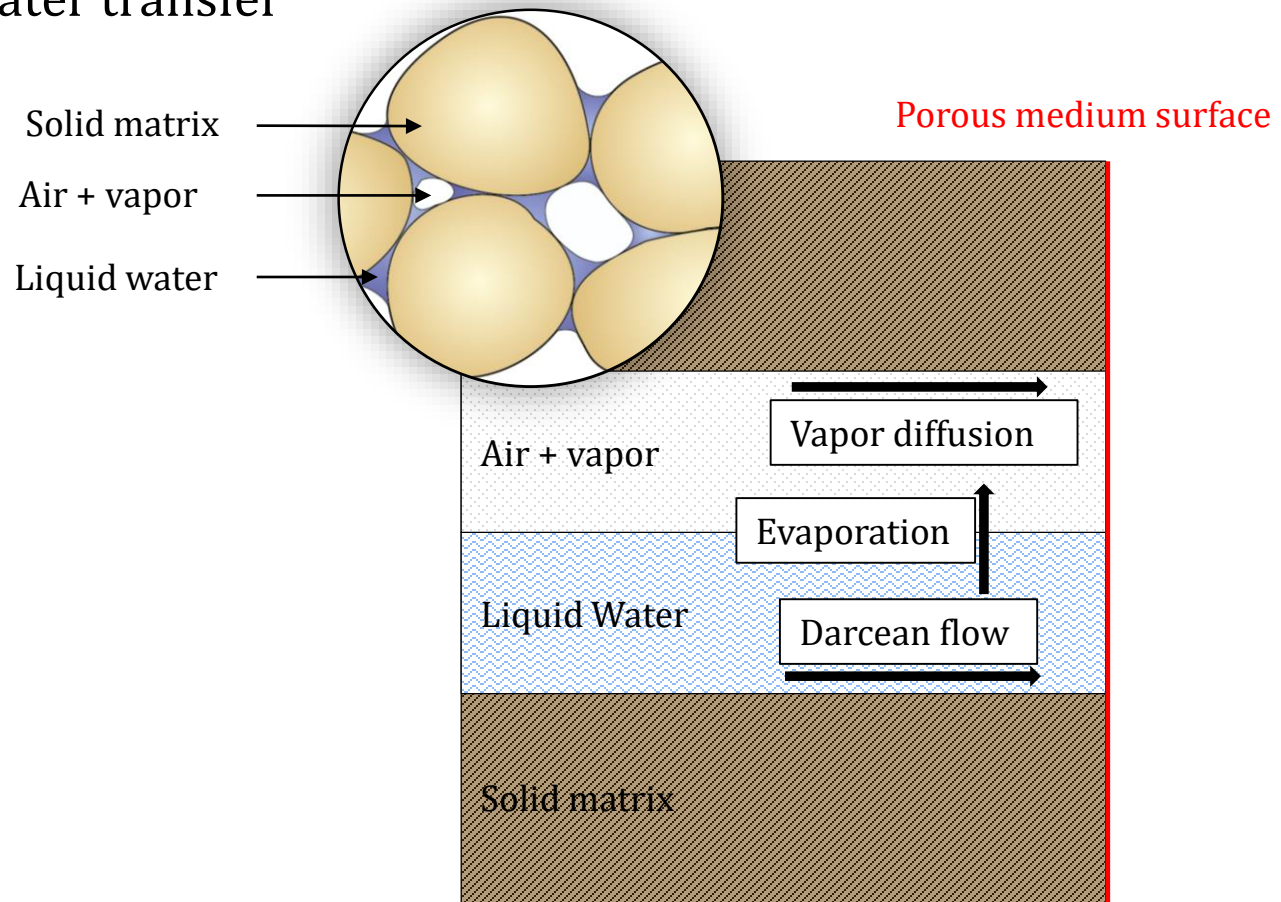
# DRYING KINETICS

- Porous medium



# DRYING KINETICS

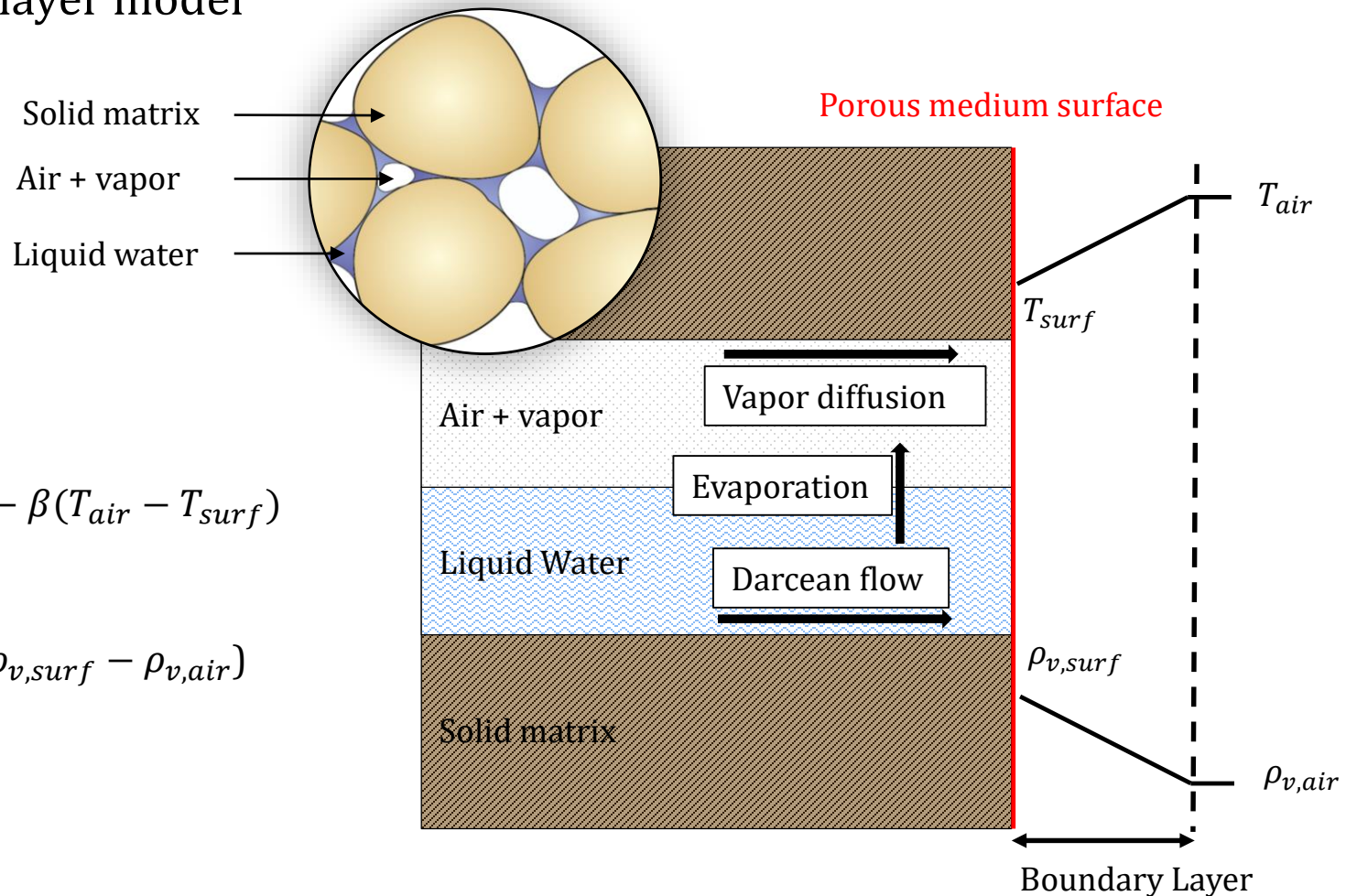
- Internal water transfer





# DRYING KINETICS

- Boundary layer model



Heat flux :

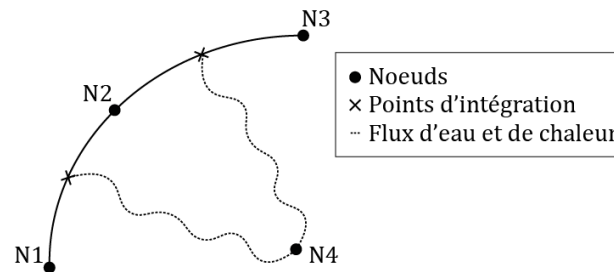
$$q_h = Lq_w - \beta(T_{air} - T_{surf})$$

Water flux :

$$q_w = \alpha(\rho_{v,surf} - \rho_{v,air})$$

# NUMERICAL STUDY OF THE DRYING KINETICS

- **Integration of limit layer model into a FEM framework :**
  - Use of a special kind of finite element :



- **Boundary conditions**

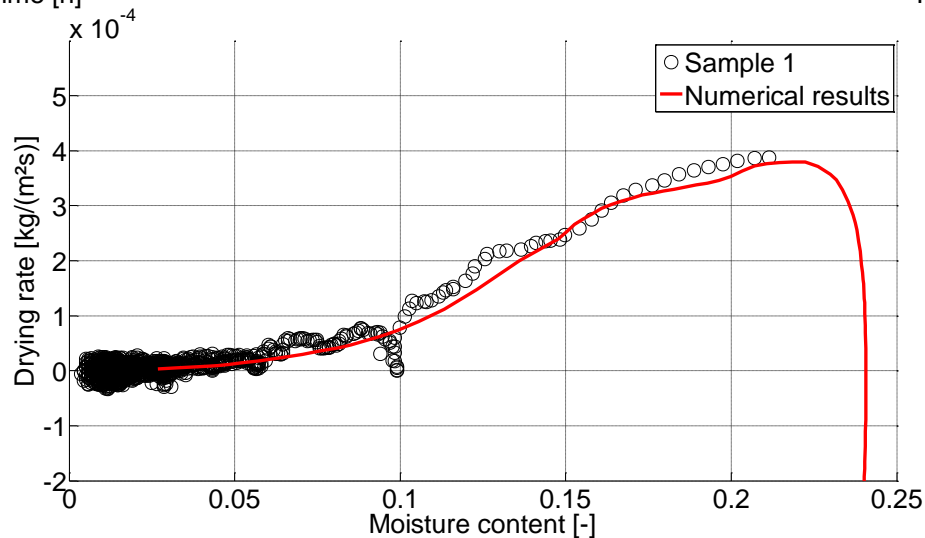
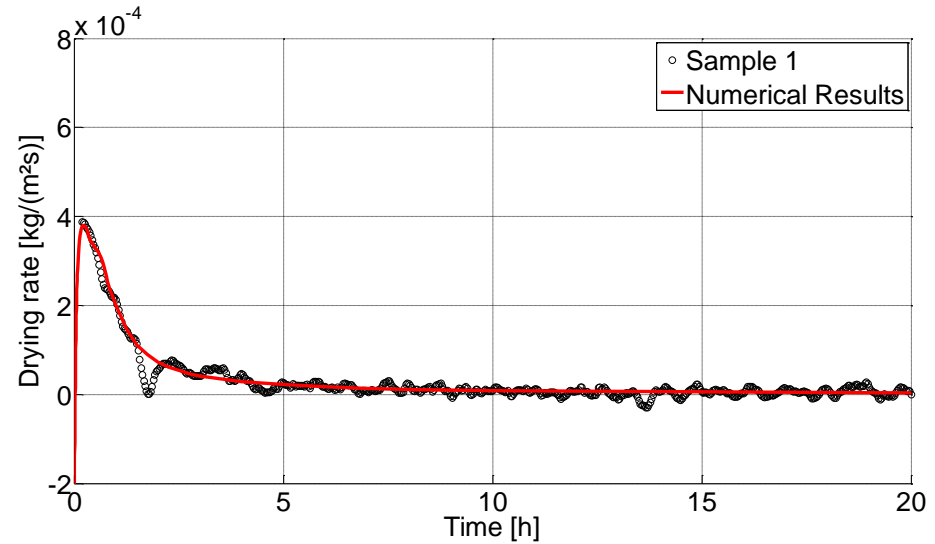
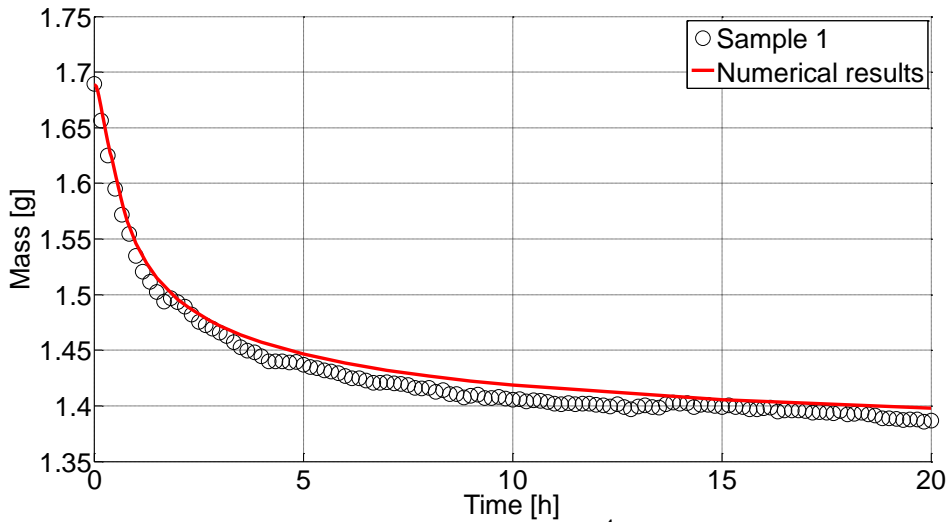
*Gerard & al, 2008*

- **Water pressure** at the environment node :  $p_c = -\frac{\rho RT}{M} \ln(HR)$
- **Temperature** at the environment node :  $T = 25^\circ\text{C}$
- **Transfer coefficients :**

$\alpha$ [m/s]	$\beta$ [W/m <sup>2</sup> /K]
0.048	53

# NUMERICAL STUDY OF THE DRYING KINETICS

## ■ Numerical results:

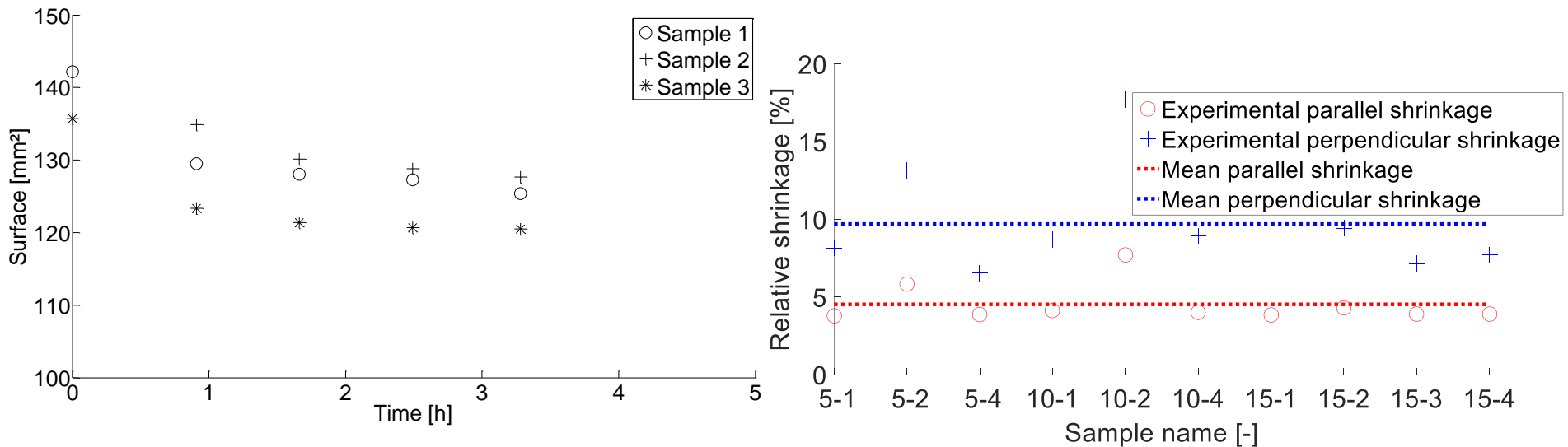


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# DRYING SHRINKAGE

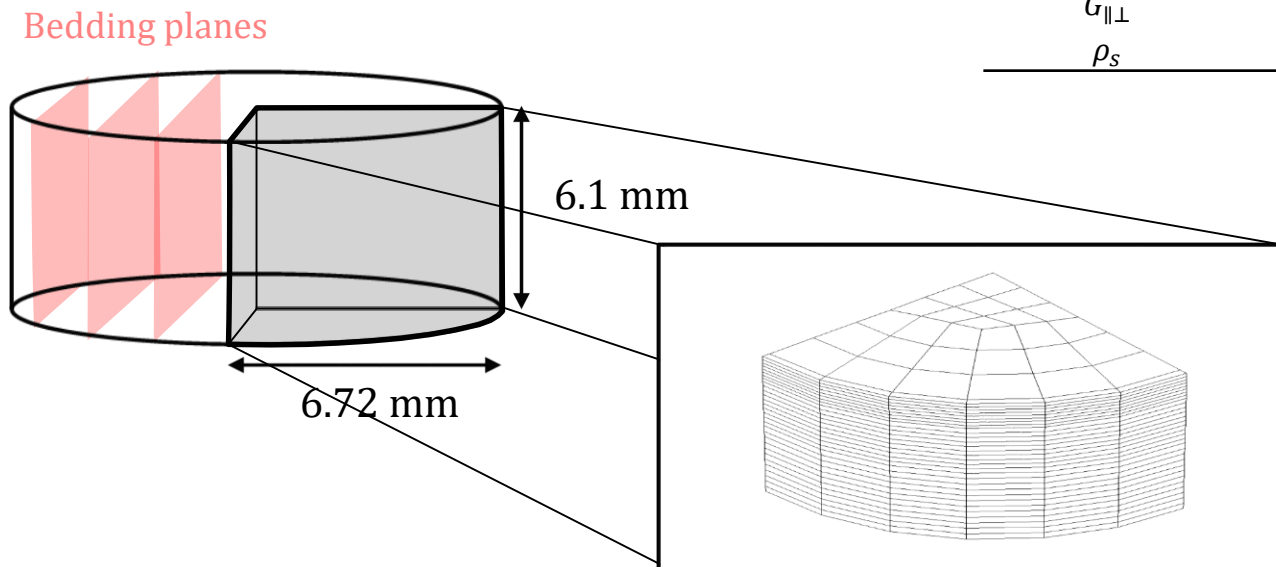
## ■ Experimental results



# NUMERICAL STUDY OF THE DRYING SHRINKAGE

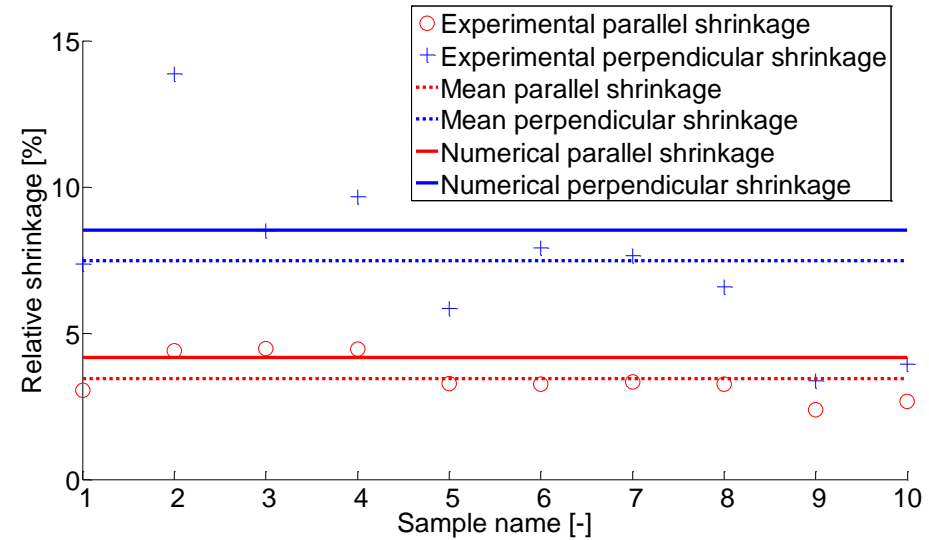
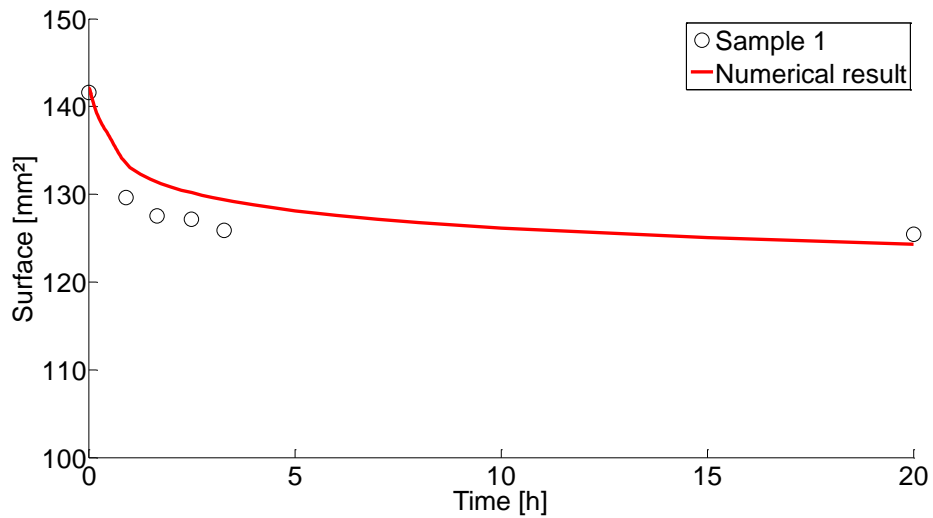
- Numerical mechanical model
  - 3D Orthotropic hydro-mechanical model

MECHANICAL PARAMETERS ( <i>DIZIER, 2011</i> )		
$E_{\parallel}$	700	[MPa]
$E_{\perp}$	350	[MPa]
$\nu_{\parallel\parallel}$	0.25	[-]
$\nu_{\parallel\perp}$	0.125	[-]
$G_{\parallel\perp}$	1.4	[MPa]
$\rho_s$	2670	[kg/m <sup>3</sup> ]



# NUMERICAL STUDY OF THE DRYING SHRINKAGE

## ■ Numerical results

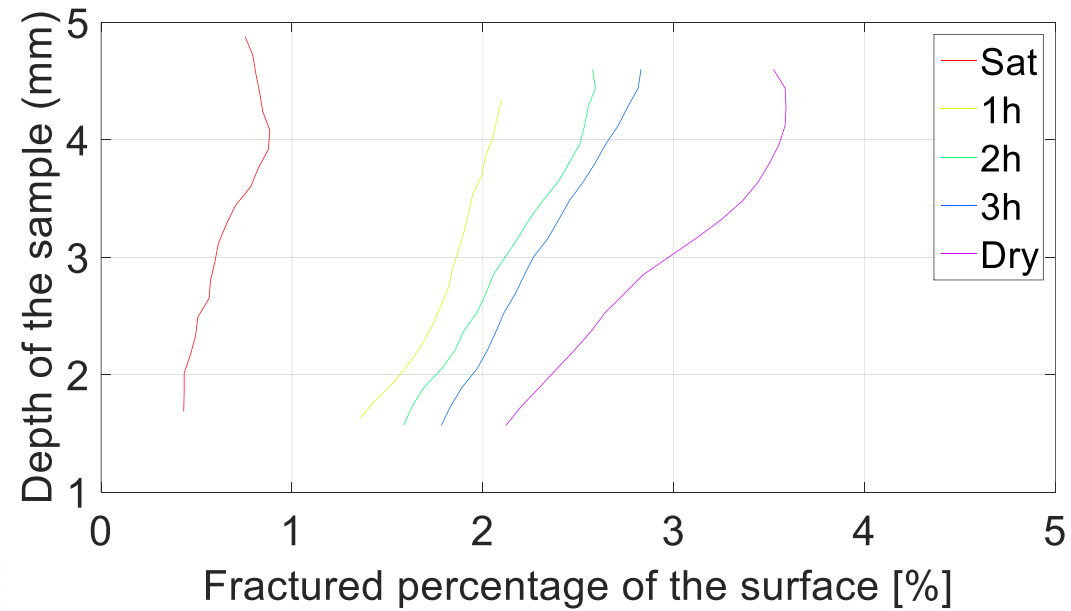
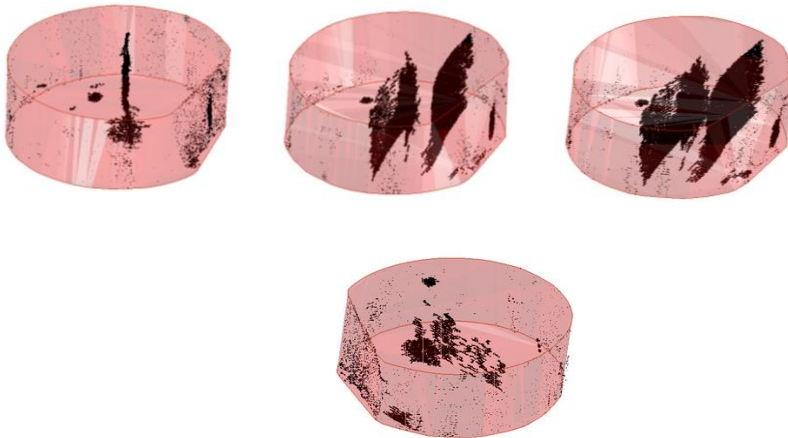


# CONCLUSION

## ■ Dessiccation cracking



Time





# REFERENCES

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- Bastiens W., Demarche M., 2003. The extension of the URF HADES: realization and observation. Proceedings of the WN'03 Conference, Tucson, USA.
- Craeye B., De Schutter G., Van Humbeeck H., Van Cotthem, 2009. *Early age behaviour of concrete supercontainers for radioactive waste disposal*. Nuclear Engineering and Design, 239, 23-35.
- Gerard P., Charlier, R, Chambon, R, & Collin, F. 2008. Influence of evaporation and seepage on the convergence of a ventilated cavity. Water resources research, 44(5), W00C02.
- Léonard A., Étude du séchage convectif de boues de station d'épuration. Suivi de la texture par microtomographie à rayons X. Thèse de doctorat, Université de Liège, Faculté des Sciences appliquées, 2003.
- SCK-CEN. R and D for the geological disposal of medium and high level waste in the Boom clay, 2009. [URLence.sckcen.be/en/Projects/Project/RD\\_waste\\_disposal/Geological\\_disposal](http://en.lence.sckcen.be/en/Projects/Project/RD_waste_disposal/Geological_disposal).

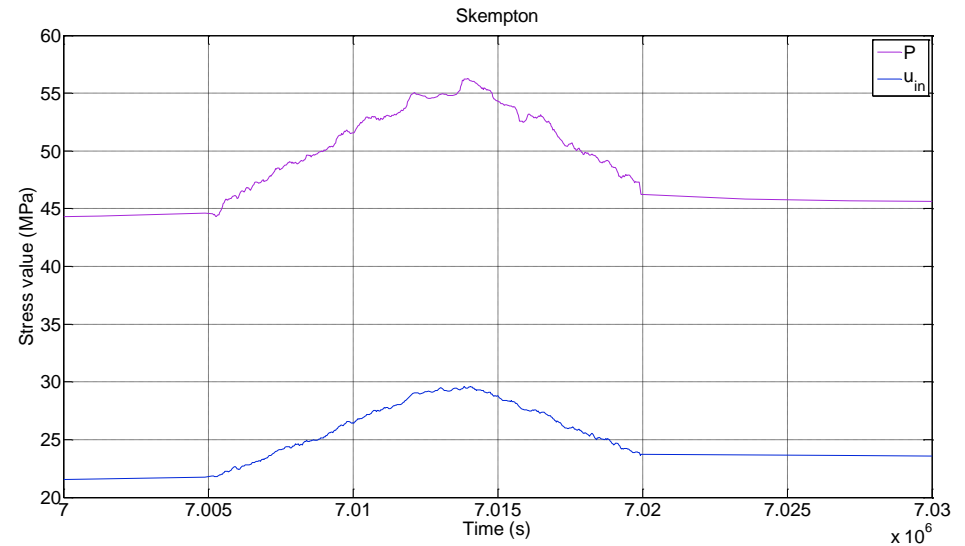
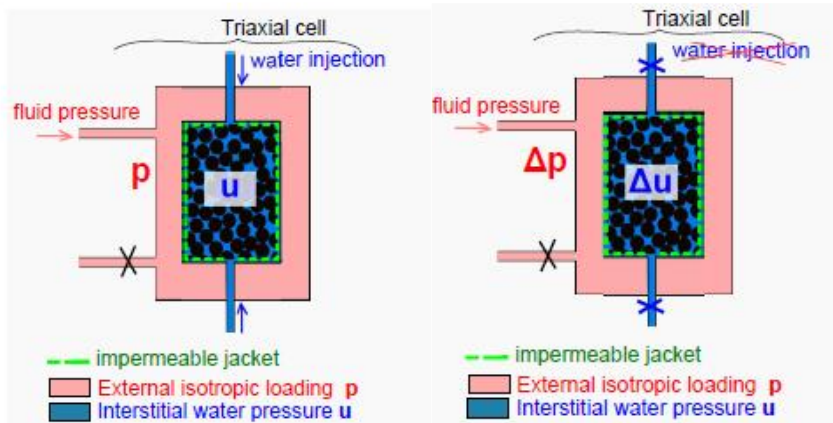
Thank you !

This work was possible thanks to the FRS-FNRS  LA LIBERTÉ DE CHERCHER

[julien.hubert@ulg.ac.be](mailto:julien.hubert@ulg.ac.be)

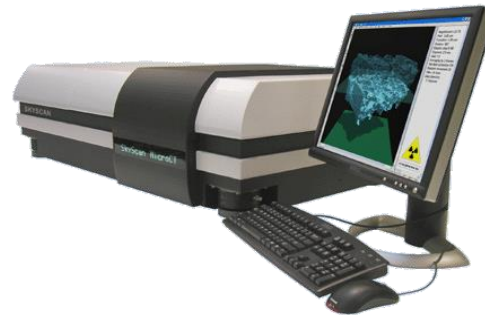
# SATURATION CONTROL

- Skempton coefficient



# MATERIALS AND METHODS

- X-Ray tomography characteristics
  - Cross section acquisition using a X-Ray microtomography



*Skyscan 1172*

Source Voltage = 100 kV

Filter = Al 0.5 mm

4x4 binning = 900x666 pixel radiograms

Pixel size = 27.27  $\mu\text{m}$

Exposure time = 510 ms

Rotation Step (deg)= 0.65

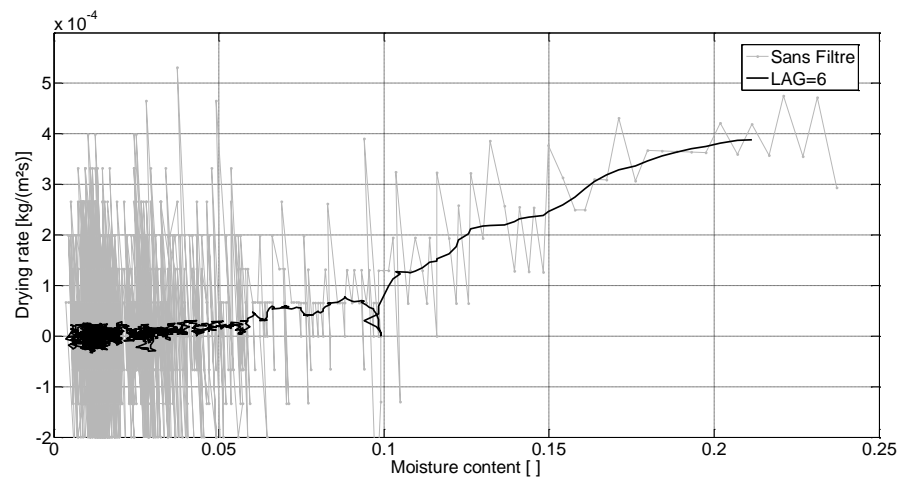
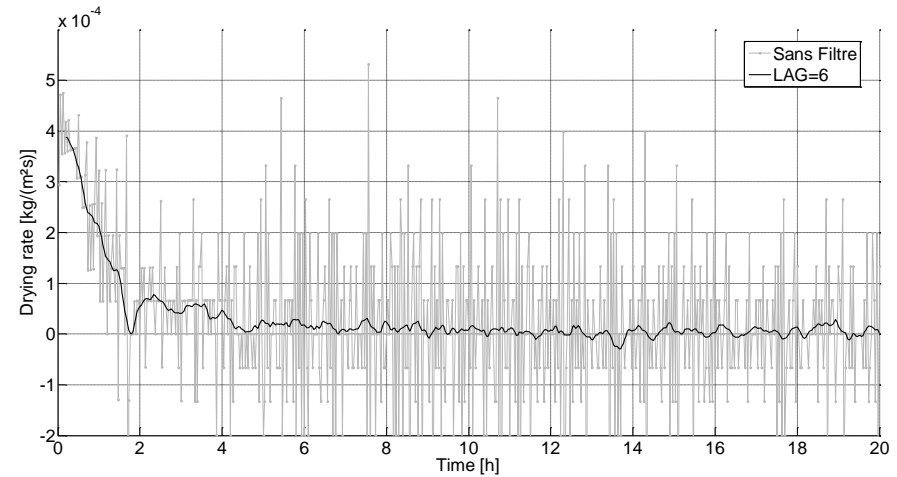
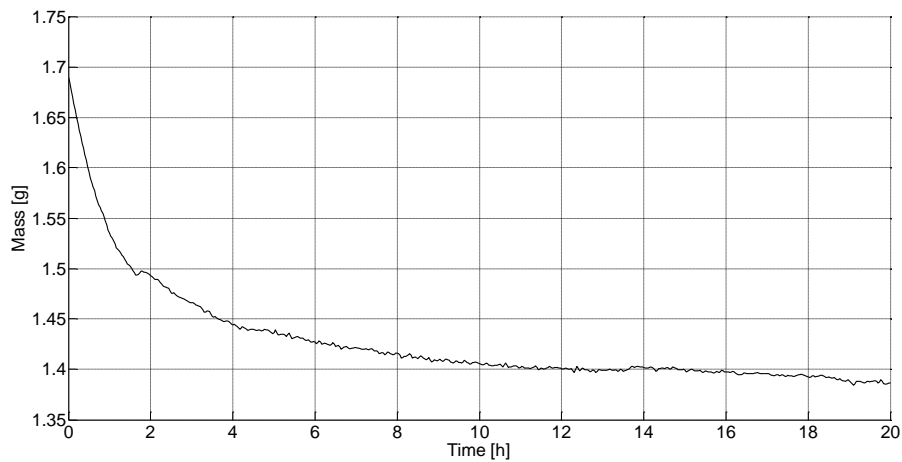
180° rotation

2 vertically-connected scans

Scan duration = 8 minutes

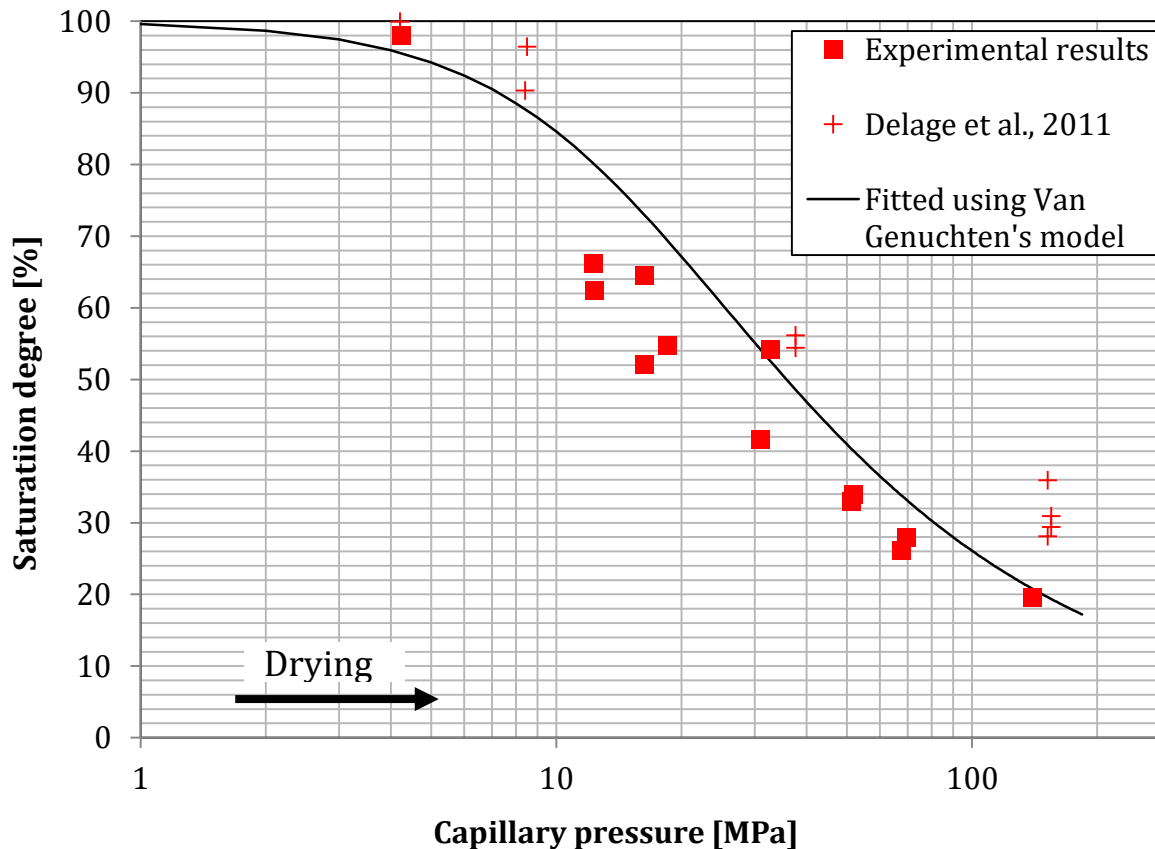
# Experimental results

## ■ Numerical filter



# WATER RETENTION CURVE

- Samples put into chamber with controlled suction (saline solution)
- Water content measured  $\Rightarrow$  saturation degree deduced



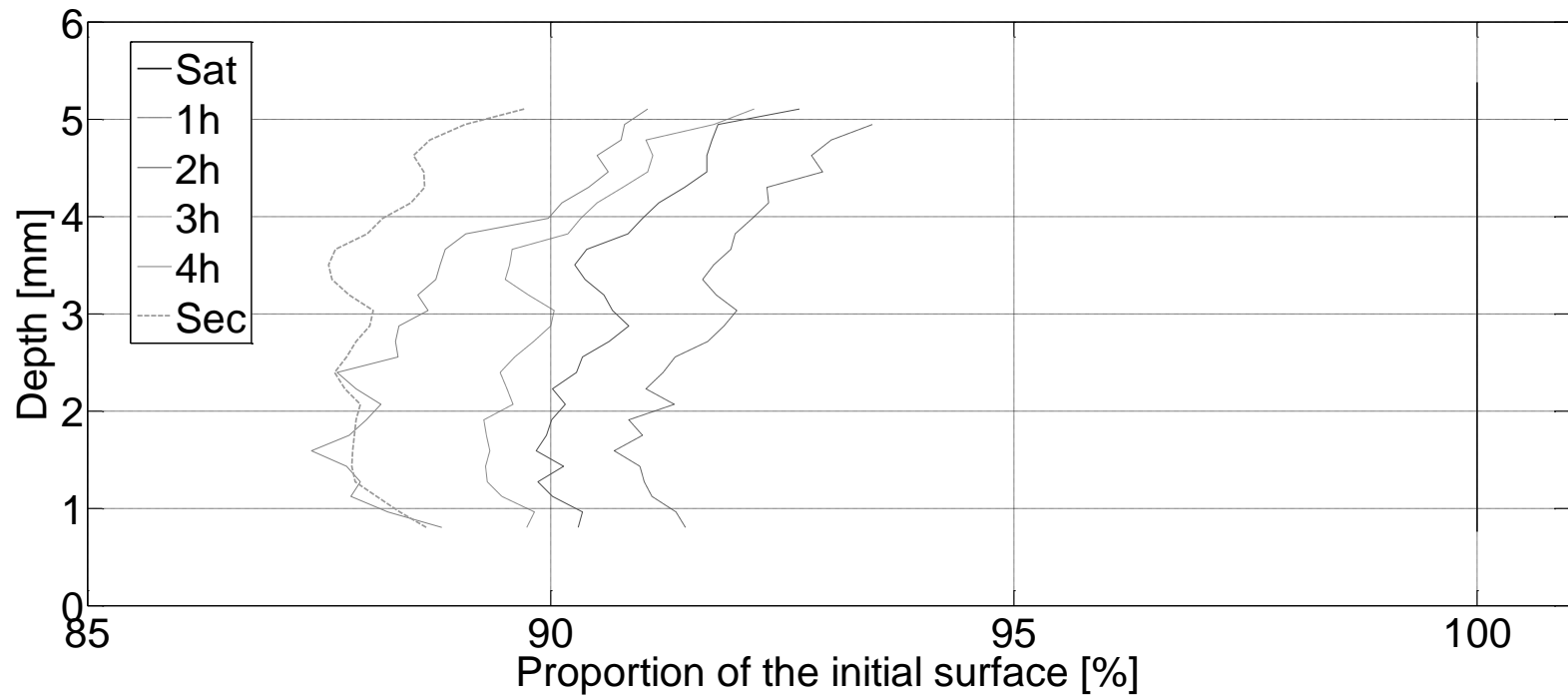
Van Genuchten formulation :

$$S_{r,w} = S_{res} + (S_{sat} - S_{res}) \left[ \left( 1 + \frac{p_c}{\alpha} \right)^{n_{vg}} \right]^{-m_{vg}}$$

VAN GENUCHTEN FORMULATION		
$S_{res}$	0	[-]
$S_{sat}$	1	[-]
$\alpha_{vg}$	15	[MPa]
$m_{vg}$	0.449	[-]
$n_{vg}$	1.70	[-]

# DRYING SHRINKAGE

- Quickly homogeneous on the whole sample



# NUMERICAL STUDY

- Parameters used :

PARAMETERS	VALUES	UNITS
HYDRAULIC PARAMETERS		
$k_{sat,\perp}$	$8.10^{-12}$	[m/s]
$k_{sat,\parallel}$	$2.10^{-12}$	[m/s]
n	0.39	[-]
MECHANICAL PARAMETERS		
$E_{\parallel}$	700	[MPa]
$E_{\perp}$	350	[MPa]
$\nu_{\parallel}$	0.25	[-]
$\nu_{\parallel\perp}$	0.125	[-]
$G_{\parallel\perp}$	1.4	[MPa]
$\rho_s$	2670	[kg/m <sup>3</sup> ]
THERMAL PARAMETERS		
$c_s$	2080	$[\frac{J}{kg * K}]$
$\rho_s$	2670	[kg/m <sup>3</sup> ]
$c_w$	4185	$[\frac{J}{kg * K}]$
$\rho_w$	1000	[kg/m <sup>3</sup> ]
$c_a$	1004	$[\frac{J}{kg * K}]$
$\rho_a$	1.2	[kg/m <sup>3</sup> ]



# NUMERICAL MODEL

- Thermal model

- Storage

$$S_T = \underbrace{nS_{r,w}\rho_w c_{p,w}(T - T_0)}_{\text{Liquid water}} + \underbrace{nS_{r,g}\rho_a c_{p,a}(T - T_0)}_{\text{Air}} + \underbrace{nS_{r,g}\rho_v c_{p,v}(T - T_0)}_{\text{Vapor}} + \underbrace{(1 - n)\rho_s c_{p,s}(T - T_0)}_{\text{Solid}} + \underbrace{nS_{r,g}\rho_v c_{p,v}L}_{\text{Vapor latent heat}}$$

- Heat flux

$$V_T = \underbrace{-\Gamma\nabla T}_{\text{Conduction}} + \underbrace{c_{p,w}\rho_w f_w(T - T_0) + c_{p,a}\rho_a f_g(T - T_0) + c_{p,v}(\rho_v f_v + i_v)(T - T_0) + (\rho_v f_v + i_v)L}_{\text{Convection}}$$