

# A NUMERICAL STUDY OF FIBER GLASS DRAWING PROCESS

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**19 October 2012**

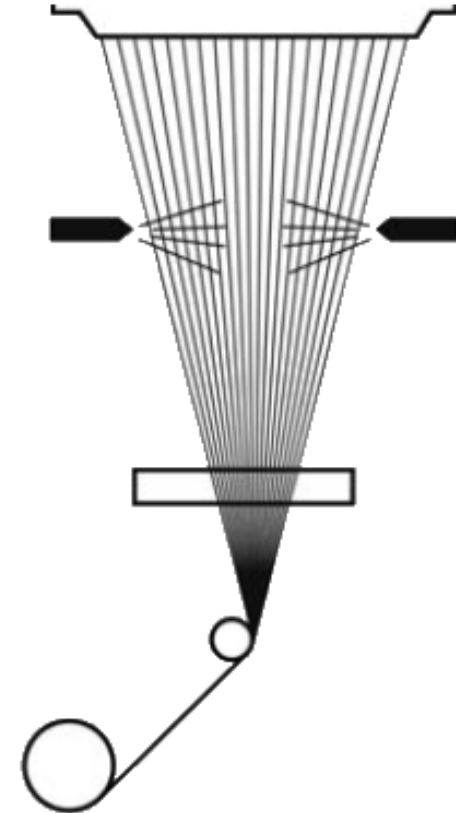
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## • General context

- Physics of fiber drawing process
  - Numerical study – Heat transfer
  - Numerical study – Flow rate
  - Conclusion
-

# Fiberization process

- Glass fibers are made by drawing thousands of fibers from a bushing plate:
  - Glass melt flows through tip
  - Forming fibers are cooled by fins and water spray
  - Coating is applied to fibers
  - Fibers are drawn by a winder
- Efficiency improvement of fiberglass drawing process is mostly driven by **fiber breakage reduction**
- Break implies :
  1. Shut down of forming station and thus **production loss**
  2. Large amount of **unrecyclable glass waste**
  3. **Barrier to optimization of** manufacturing process



# Goal and impact of research

## Goal

- Understand the **origins of fiber breaking** during forming process
- Identify strategy **to reduce** as much as possible the **breaking rate**

## Impact

- **Fiber drawing process**
  - Improved numerical modeling and simulations
  - Better understanding of breaking mechanisms
- **Manufacturing process**
  - Energy and waste reduction
  - New design of tips, bushing plate, cooling fins ...
  - Lower costs to produce the same quantity of fiber glass

# Pathway to improved efficiency

Improve knowledge of  
fiber drawing process

- Physical models
- Simulations
- Experimental studies
- Parameter studies

Understand underlying  
physics of filament  
breaking

- Characterize breaking:  
When? Where? Why?
- Probability of failure
- Experimental studies

Devise strategy for  
reducing breaking rate

- New design of  
bushing unit
- Modification of  
operating windows
- ...

# Physics of one fiber forming

## Heat transfer

## Fluid flow

- Radiation
- Convection
- Conduction



→ Glass melt  
Viscous flow

$$T > T_g$$

- Convection
- Conduction



→ Glass transition  
Viscoelastic flow

$$T \approx T_g$$

- Convection
- Conduction



→ Glassy state  
Elastic solid

$$T < T_g$$

# Governing glass flow equations

## Governing viscous flow equations: *Newtonian flow*

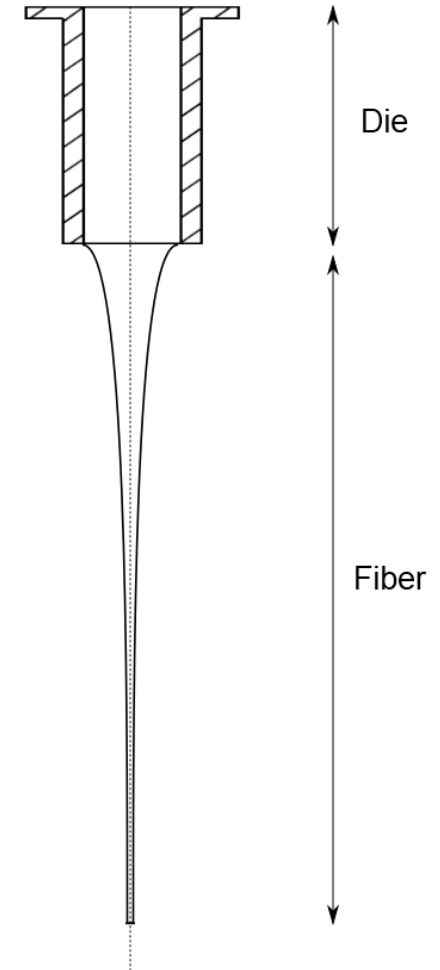
Mass conservation:  $\frac{D\rho}{Dt} = 0$

Momentum conservation:  $\frac{D(\rho\mathbf{v})}{Dt} = \nabla \cdot \boldsymbol{\sigma} + \mathbf{f}$

Energy conservation:  $\frac{D(\rho c_p T)}{Dt} = \boldsymbol{\sigma} : \nabla \mathbf{v} - \nabla \cdot \mathbf{q} + r$

## Assumptions:

- Fulcher viscosity equation:  $\eta = 10^{-A + \frac{B}{T-T_0}}$
- Internal radiation, gravity and viscous heating neglected
- External temperature remains constant around fiber



# Boundary conditions

## Inlet

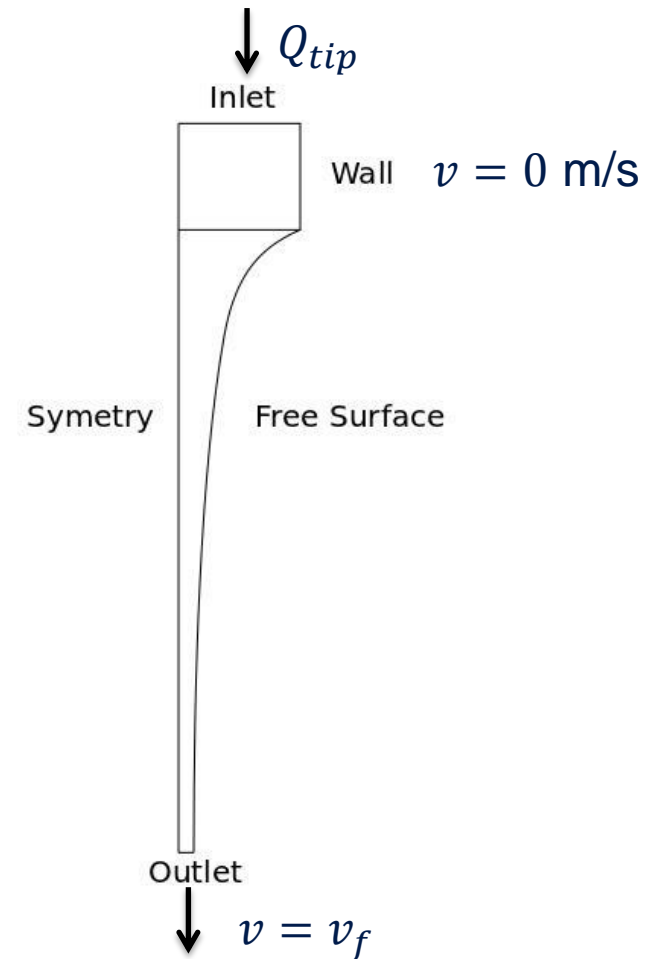
- Volumetric flow rate:  $Q_{tip} = \frac{\pi}{8\eta} \left( -\frac{\partial p}{\partial z} \right) r_0^4$
- Constant temperature

## Free surface

- Heat flux:  $q = h(T - T_0) + \epsilon\sigma(T^4 - T_0^4)$
- Kase-Matsuo convective coefficient:  $h = \frac{0.42 k_a}{D} \left( \frac{u D}{\mu_a} \right)^{0.334}$
- Surface tension:  $\gamma$  constant

## Outlet

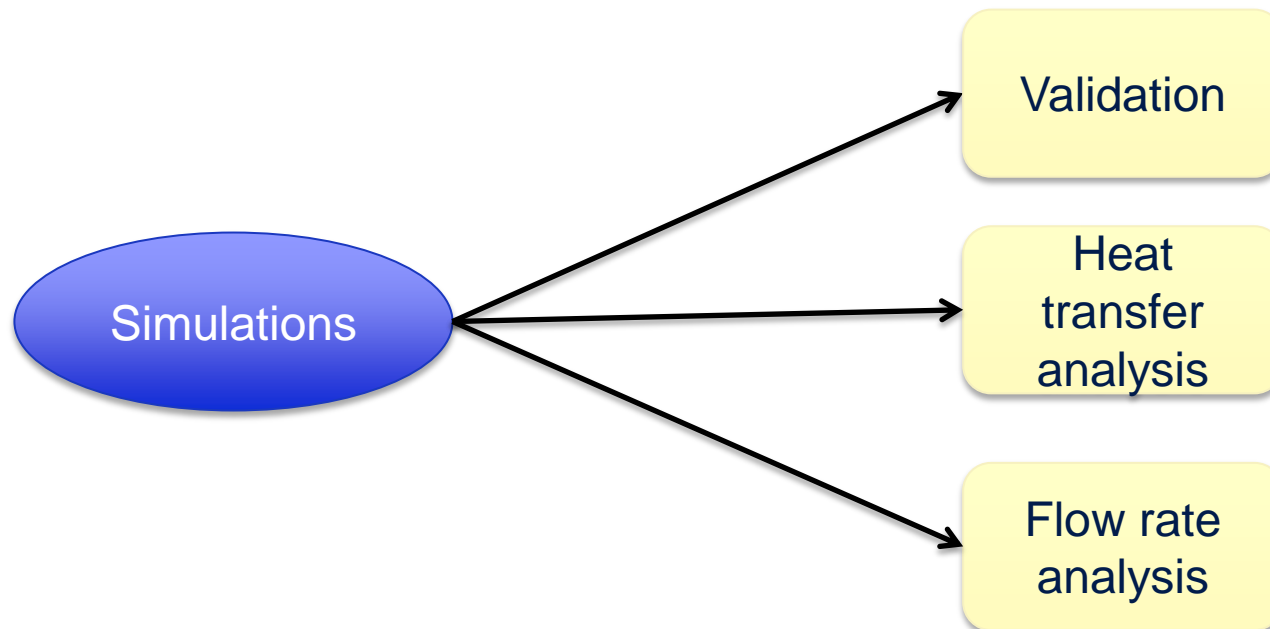
- Drawing velocity:  $v = v_f$

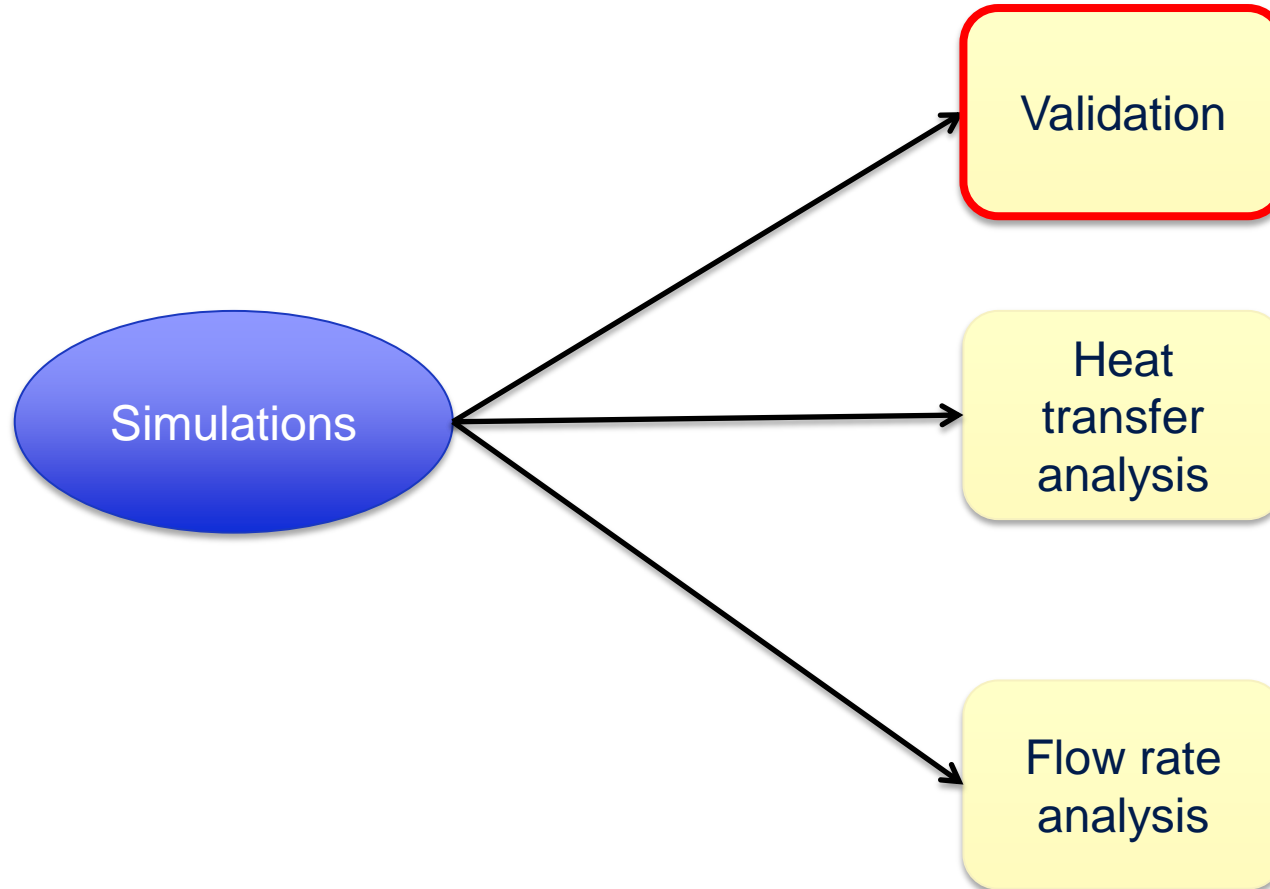




# Numerical study - Plan

- Governing equations are solved numerically with finite elements method with computer simulations
- Simulations performed with **ANSYS Polyflow** software
- Three sets of simulation:





# Initial validation of numerical approach

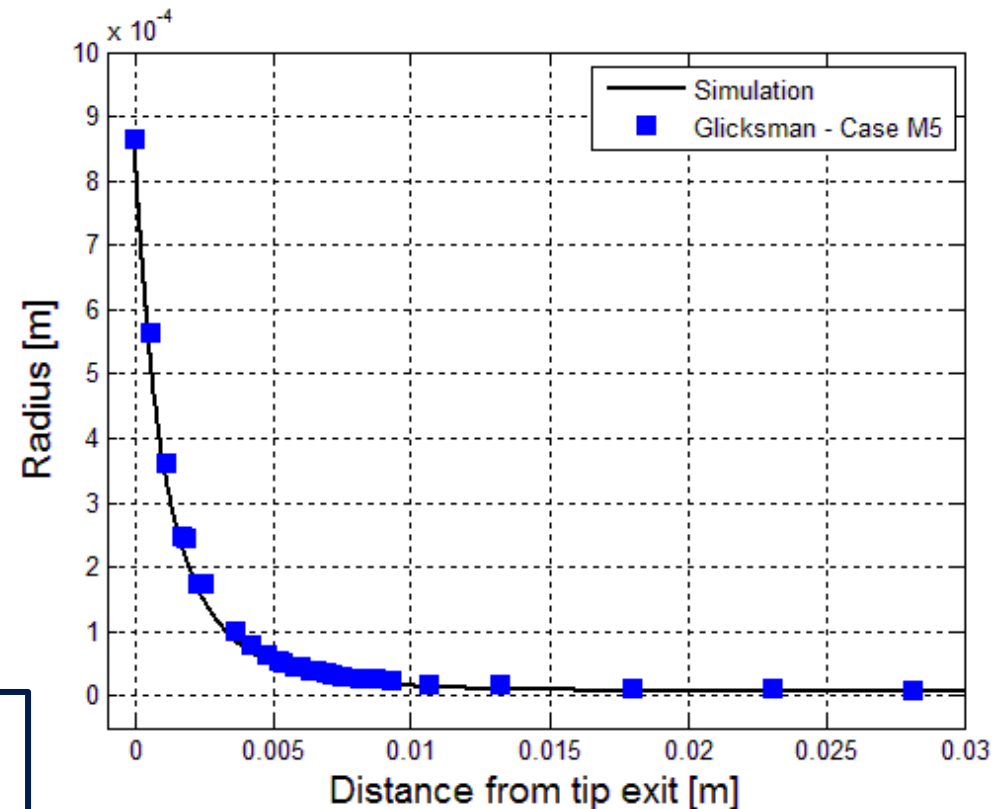
Validation from experimental data (*L. R. Glicksman, PhD thesis, MIT, 1964*)

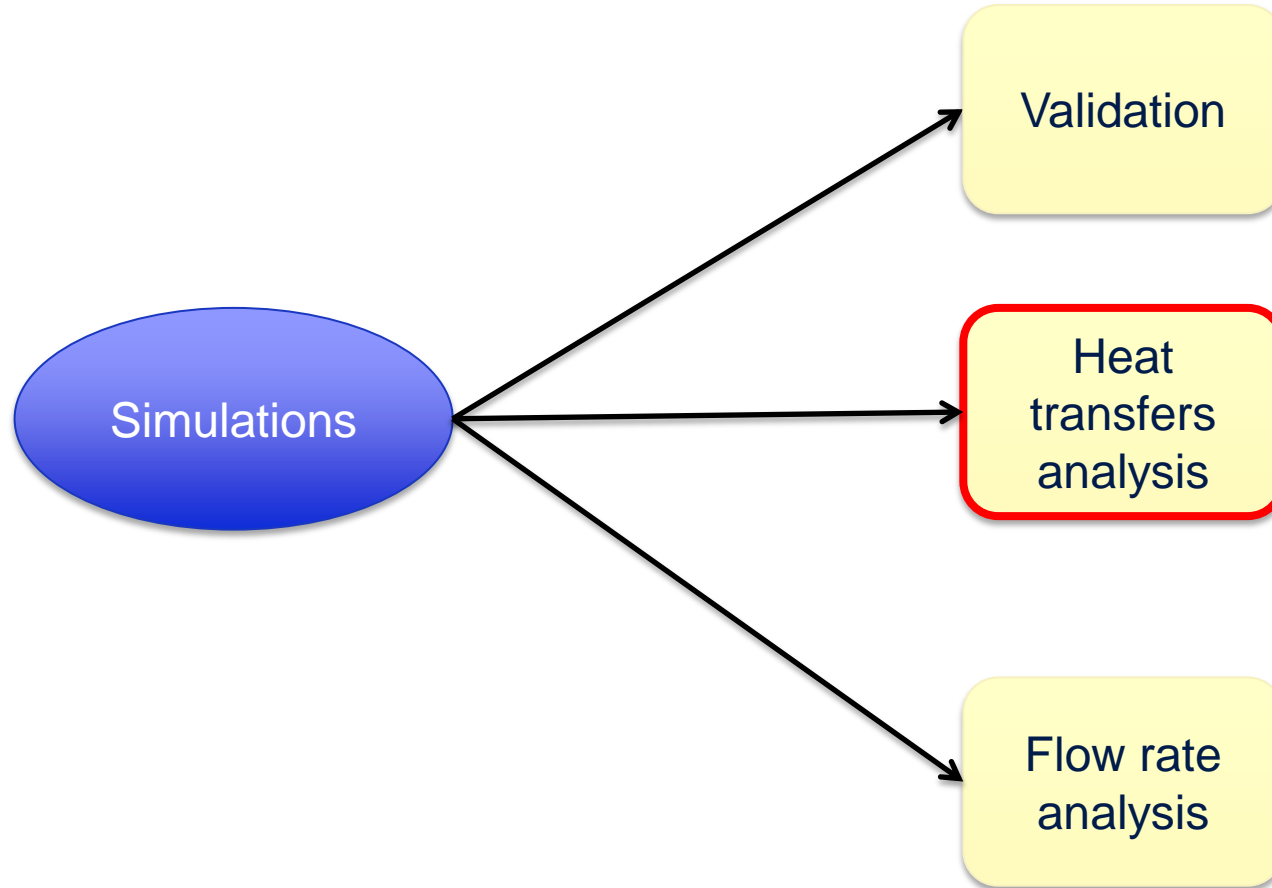
## Case study

Material	Glass M5
$T_0$	1227 °C
$Q_{in}$	$3.17 \cdot 10^9 \text{ m}^3/\text{s}$
$v_f$	$25.88 \text{ m}^3/\text{s}$

→ **Good agreement between simulation and experimental data.**

## Fiber radius attenuation





# Heat transfer study

Hypothesis : External temperature of environment  $T_{ext}$  remains constant near tips exit

- Heat fluxes acting on fiber surface come from **convection** and **radiation**:

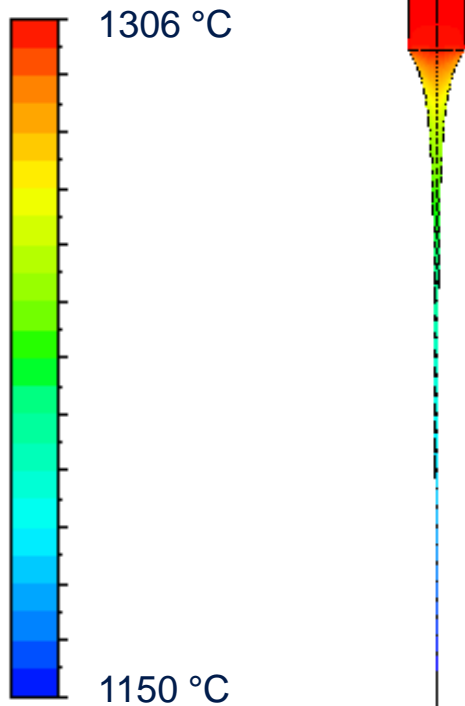
$$q = \underbrace{h(T - T_{ext})}_{\text{Convection}} + \underbrace{\epsilon\sigma(T^4 - T_{ext}^4)}_{\text{Radiation}}$$

- Kase-Matsuo convective coefficient:  $h = \frac{0.42 k_a}{D} \left( \frac{u D}{\mu_a} \right)^{0.334}$
- Convection coefficient is governed by:

- Fiber radius
- Fiber velocity
- Air properties

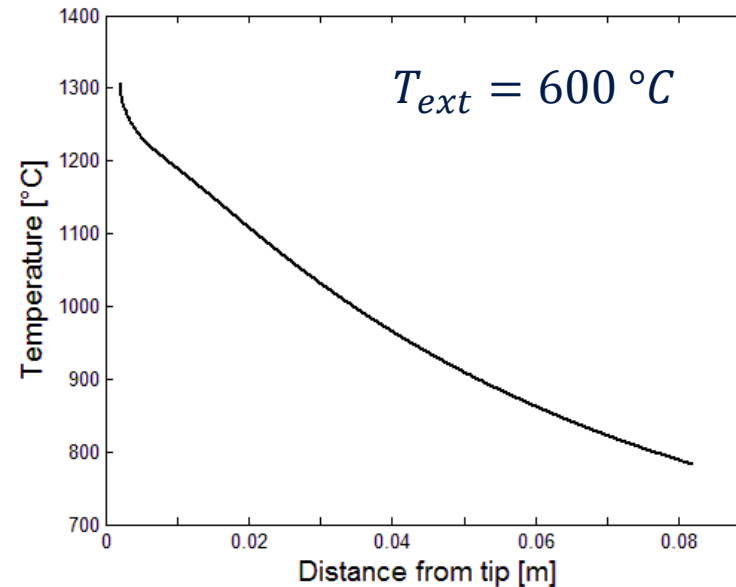
# Fiber temperature field

Temperature Field



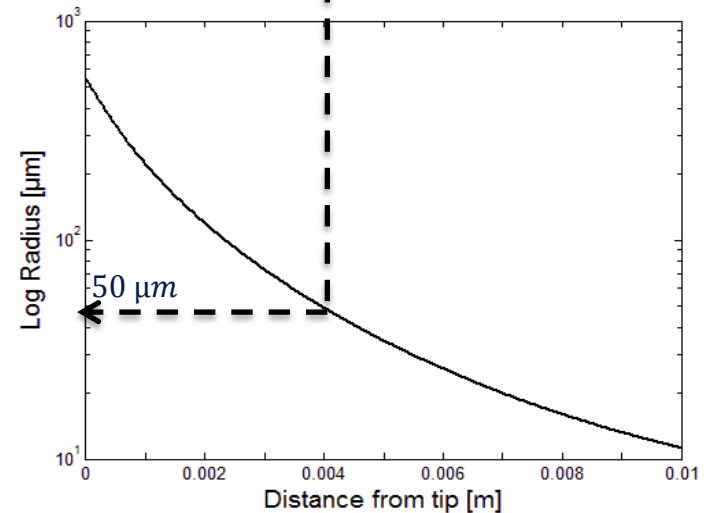
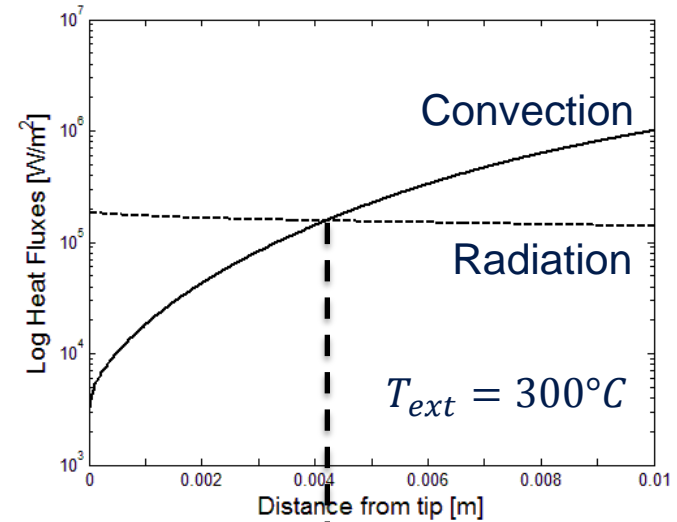
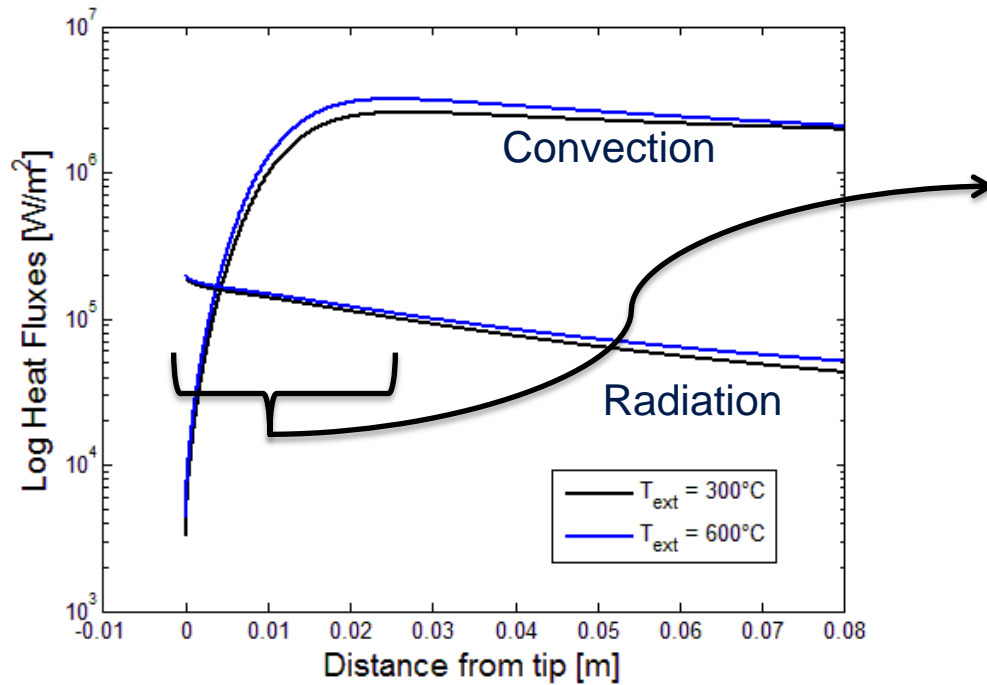
Advantex® Glass  
 $v_f = 21\text{m/s}$   
Fiberization at log 2.7

Temperature profile along the fiber boundary



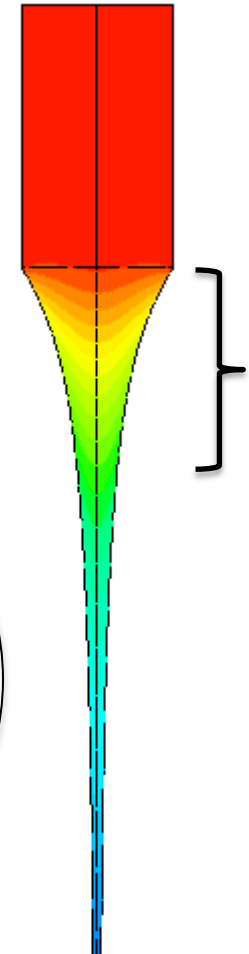
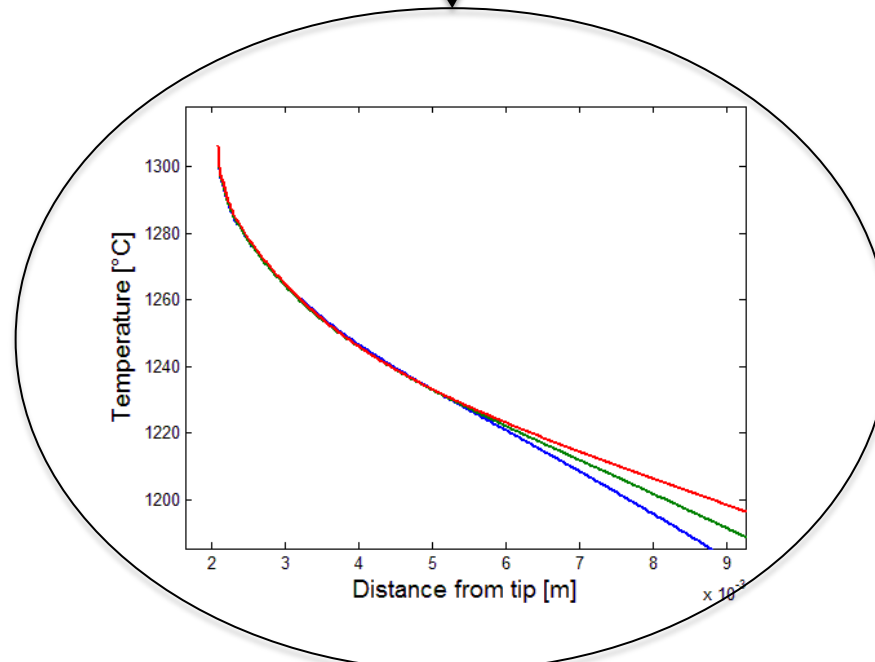
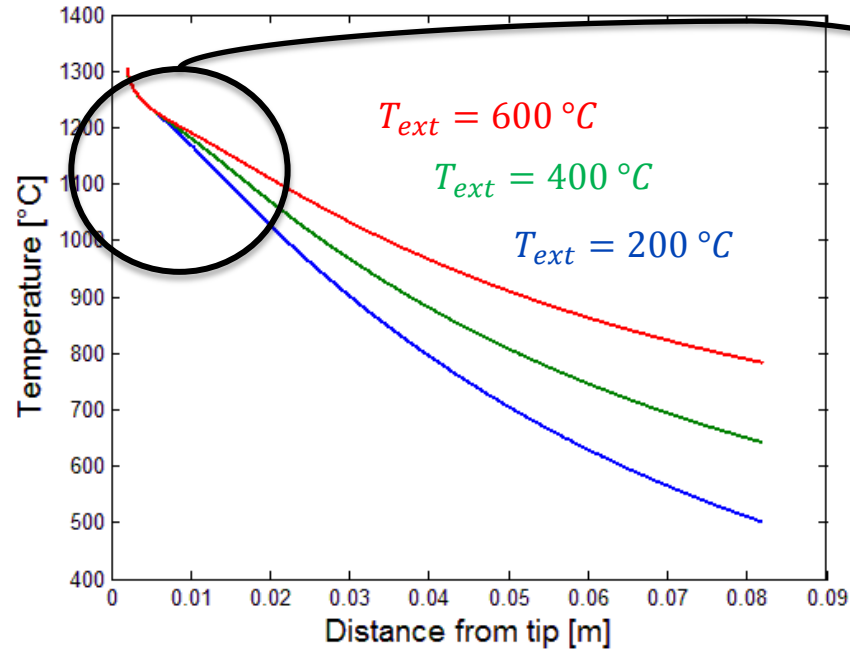
- What is the impact of the external environment?
- Which heat transfer mechanism is the most important?
- Which assumptions are the most critical?

# Radiation vs. convection



- Convection dominates very rapidly ( $\sim 1$  cm from tip)
- Attenuation of fiber radius occurs when radiation dominates

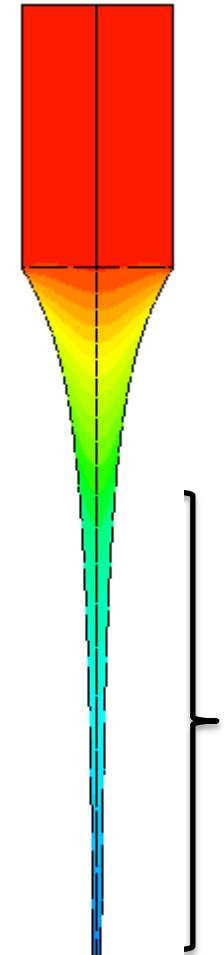
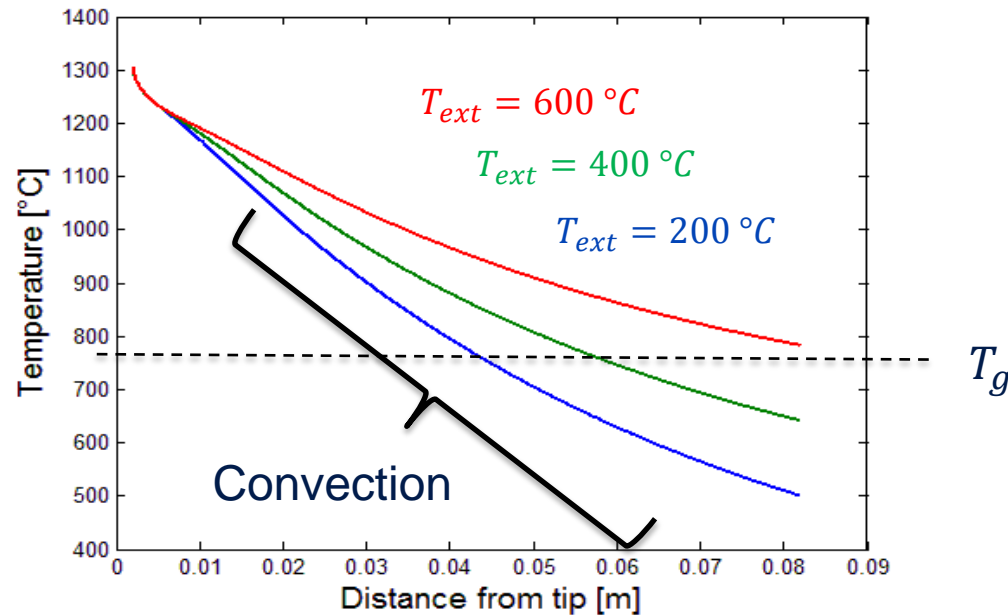
# Impact of external temperature : radiation part



- $T_{ext}$  has no impact when radiation dominates
- Fiber cooling at these temperature is governed by emissivity of glass melt

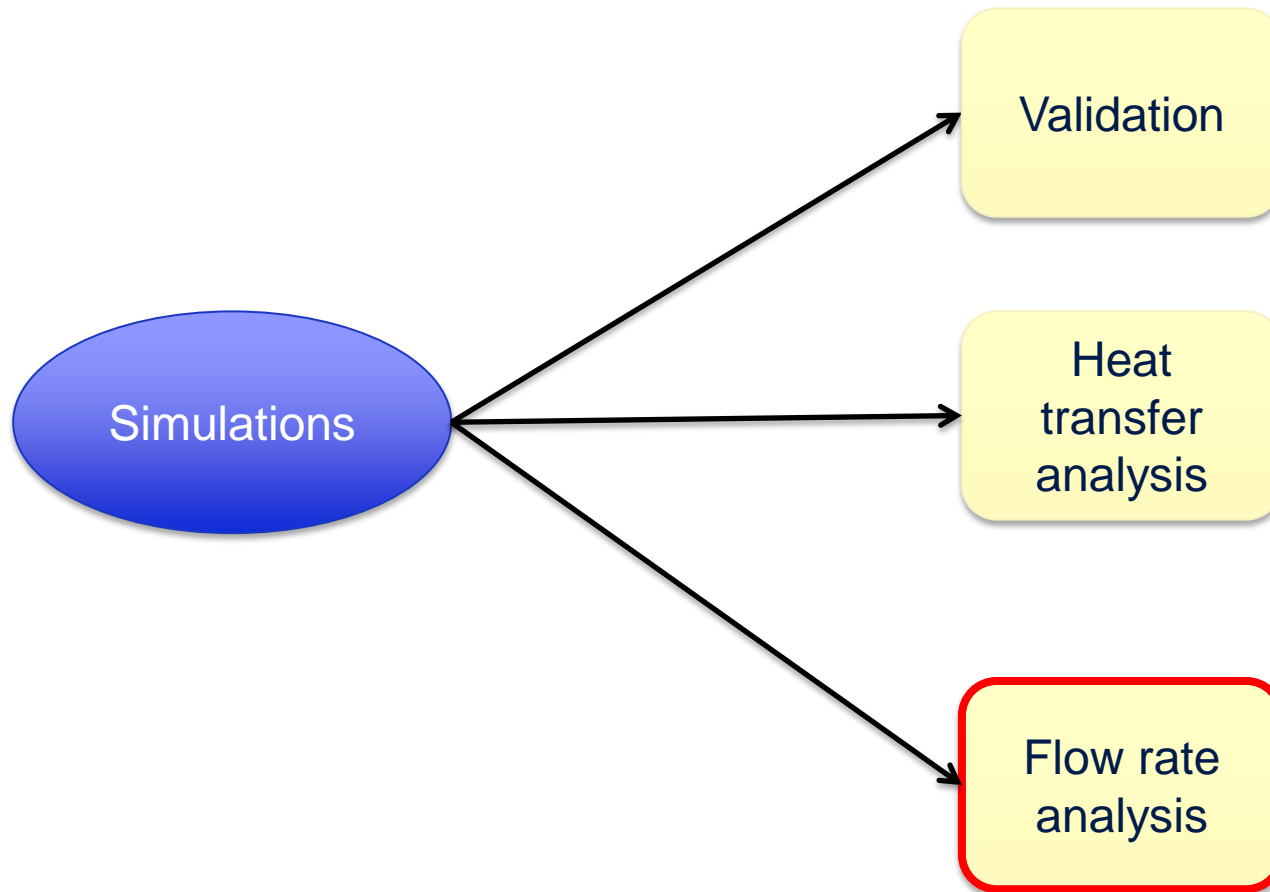


# Impact of external temperature : convection part



- $T_{ext}$  has an important impact on cooling in case of convection
- Fiber cooling at these temperature is governed by air environment
- $T_g$  does not occurs at the same distance
- Hypothesis of  $T_{ext}$  constant becomes not relevant at lower temperature

**→ more accurate if  $T_{ext}$  remains no constant**



# Flow rate impact

Flow rate inside the tip can be described by *Hagen-Poiseuille* law as:

$$Q_{tip} \sim \beta \frac{1}{8\eta} \left( -\frac{\partial p}{\partial z} \right)$$

Main parameters controlling flow rate:

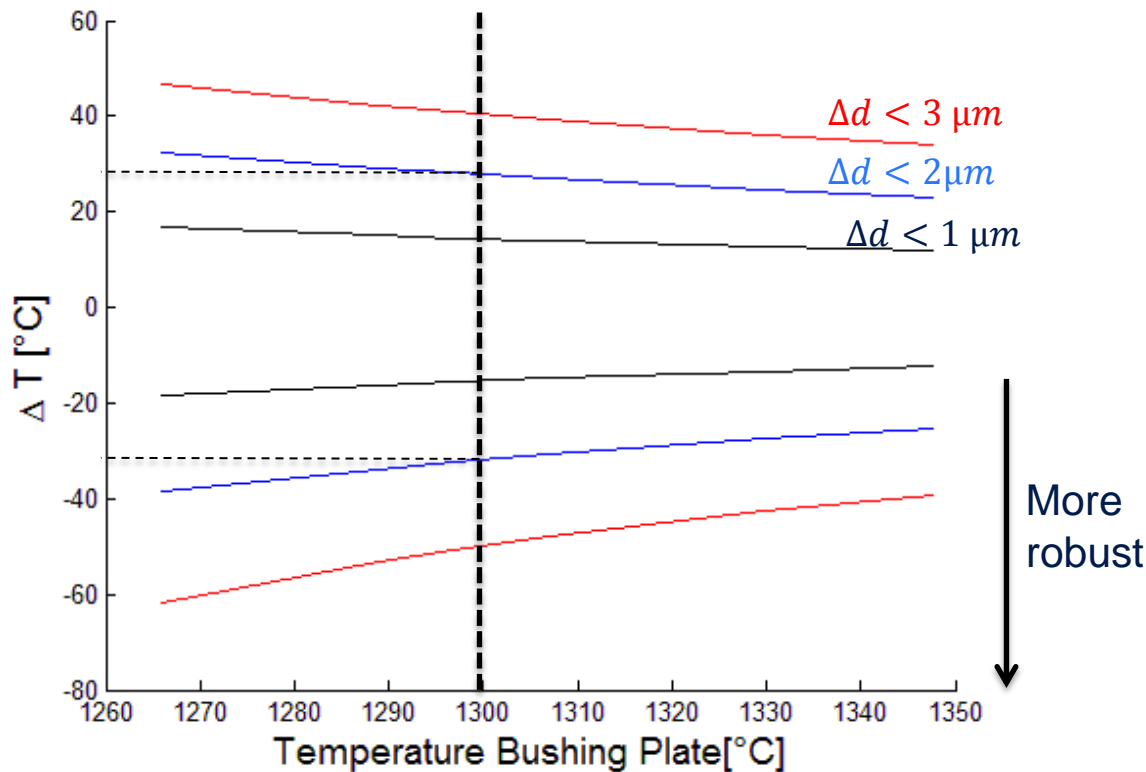
- Tip temperature:  $\eta = \eta(T)$
  - Tip shape:  $\beta$
  - Glass height (hydrostatic pressure):  $-\partial p / \partial z$
- 
- Tip shape and glass height remains (almost) constant on the bushing plate
  - Tip temperature has large impact on:
    - Fiber diameter quality
    - Fiber cooling

# Flow rate impact

Bushing plate may exhibit non-homogeneous temperature :  $T + \Delta T$

→ What is the impact of  $\Delta T$  on fiber diameter?

Maximum  $\Delta T$  admissible for fiber diameter distribution given



- Non-linear variation due to viscosity law
- unsymmetrical relative to  $\Delta T = 0 \text{ } ^\circ\text{C}$

Goal :  $d_{fiber} = 10 \mu m \pm 2 \mu m$

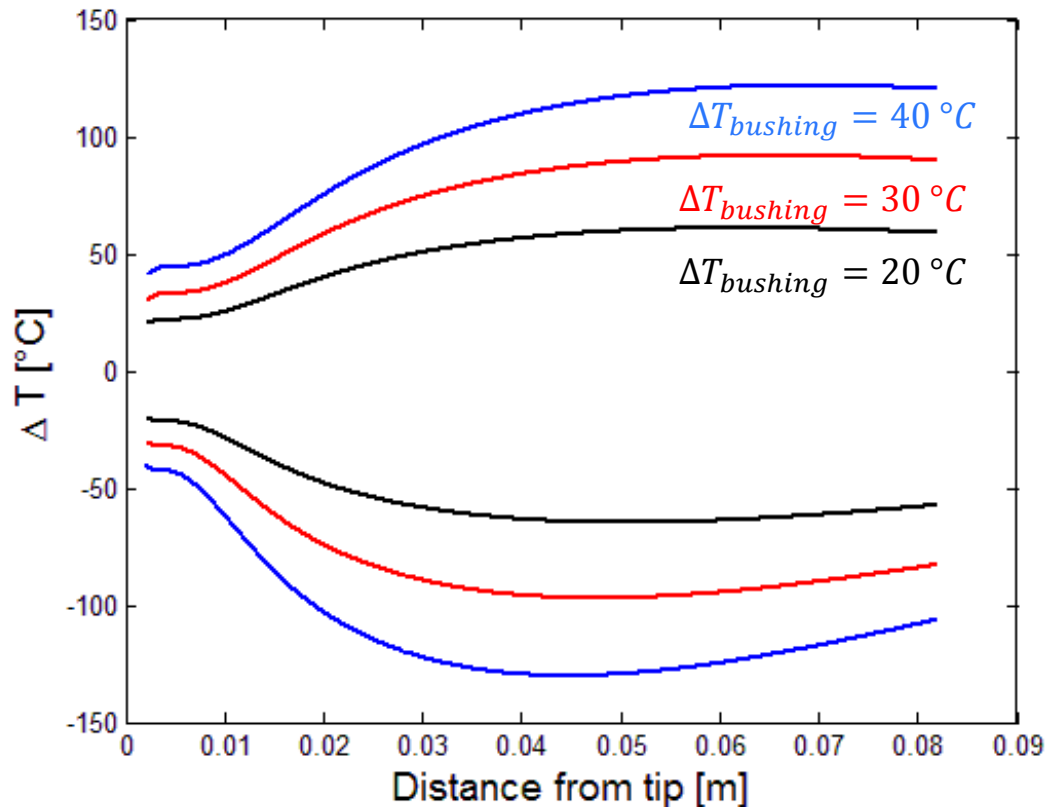
$T = 1300 \text{ } ^\circ\text{C}$

$$\Rightarrow \Delta T = \begin{cases} +28^\circ\text{C} \\ -32^\circ\text{C} \end{cases}$$

# Flow rate impact

→ How does  $\Delta T_{bushing}$  impacts on fiberization and fibers cooling ?

$\Delta T$  between two fibers along axial component



- Temperature between two fibers may varies since tip plate exhibits  $\Delta T_{bushing}$
- $\Delta T_{fiber}$  is amplified when fibers are cooling
- $\Delta T_{fiber}$  can reach  $130^\circ\text{C}$  at  $z = 0.04\text{ m}$

→ **Important to remove inhomogeneous heat pattern on bushing plate.**

# Conclusion

- Numerical simulations are very useful to understand physical mechanisms of fiber forming:
  - Radiation seems to be more important very close to the tip
  - Convection becomes dominant very quickly due to the decrease in fiber radius
  - Heat pattern of bushing plate has to be as homogenous as possible to reduce different cooling rates between fibers, and thus a broad diameter distribution
  
- Mathematical model could be improved using a more complex model for the air environment around the fiber
  
- **This tool provides a first step to reach the fundamental understanding of fiber breaking**

# Further work

## Physical model of glass fiber drawing

- Take in account viscoelasticity
- Take in account internal radiation heat transfer
- Study unsteady effects (drawing resonance)
- Study impact of uncertainties on simulation results

## Experimental devices

- Study air environment around fiber
- Link data to physical model
- And ... **characterize of fiber breaking by several experiments**